

Reinhold Environmental Ltd.



2010 NO_x-Combustion Round Table & Expo Presentation

February 8 & 9, 2010

Chattanooga, TN

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Boiler, Economizer Cleaning 101

**2010 NOx – Combustion Round Table
Chattanooga**

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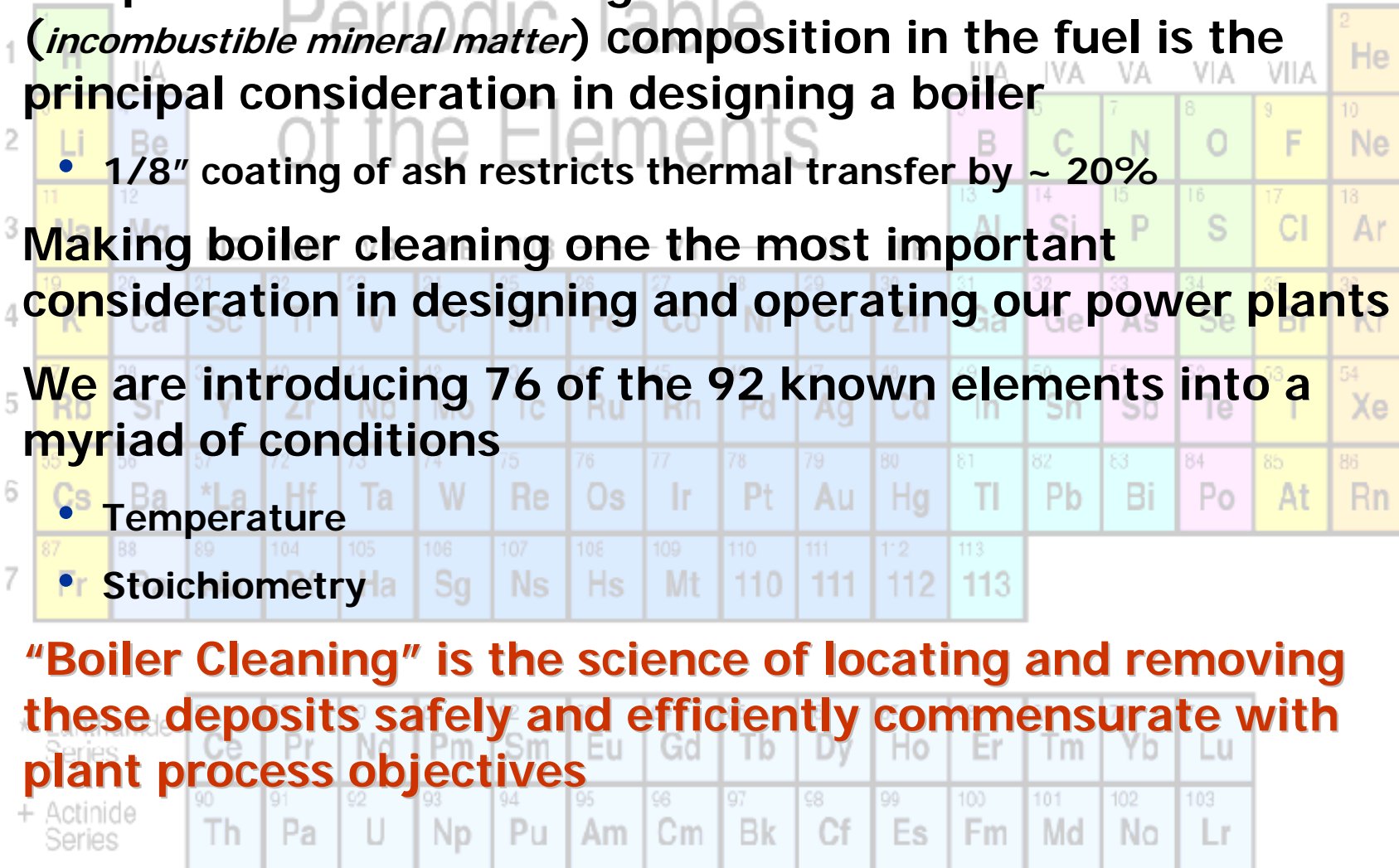
Today Focus on Boiler Cleaning

- After 90 years of dormancy we have rapidly advanced boiler cleaning technology in the past 10 years
- Culminating with the current state-of-the-art of **Intelligent Sootblowing (ISB)**
- Today we would like to present overviews of:
 - **Impact of Cleanliness on Process**
 - ⇒ Fuel changes
 - ⇒ Fuel quality
 - ⇒ Efficiency
 - ⇒ Process interruption
 - ⇒ Air quality
 - **Ash Removal Mechanisms**
 - **Ash Removal Technology**
 - **Controlling Cleanliness**



Boiler Cleaning and Boiler Design

- The published boiler design handbooks tell us that the ash (*incombustible mineral matter*) composition in the fuel is the principal consideration in designing a boiler
 - 1/8" coating of ash restricts thermal transfer by ~ 20%
- Making boiler cleaning one the most important consideration in designing and operating our power plants
- We are introducing 76 of the 92 known elements into a myriad of conditions
 - Temperature
 - Stoichiometry
- **“Boiler Cleaning” is the science of locating and removing these deposits safely and efficiently commensurate with plant process objectives**



Periodic Table of the Elements

1	H	He																	2
2	Li	Be	B	C	N	O	F	Ne											10
3	Na	Mg	Al	Si	P	S	Cl	Ar											18
4	K	Ca	Sc	Ti	V	Cr	Mn	Fe	Cu	Zn	Ga	Ge	As	Se	Br	Kr	36		
5	Rb	Sr	Y	Zr	Nb	Mo	Tc	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	Te	I	Xe	54
6	Cs	Ba	*La	Hf	Ta	W	Re	Os	Ir	Pt	Au	Hg	Tl	Pb	Bi	Po	At	Rn	86
7	Fr	Ra	†Ac	Rf	Db	Sg	Bh	Hs	Mt	110	111	112	113						118
		+ Lanthanide Series																	
		+ Actinide Series																	

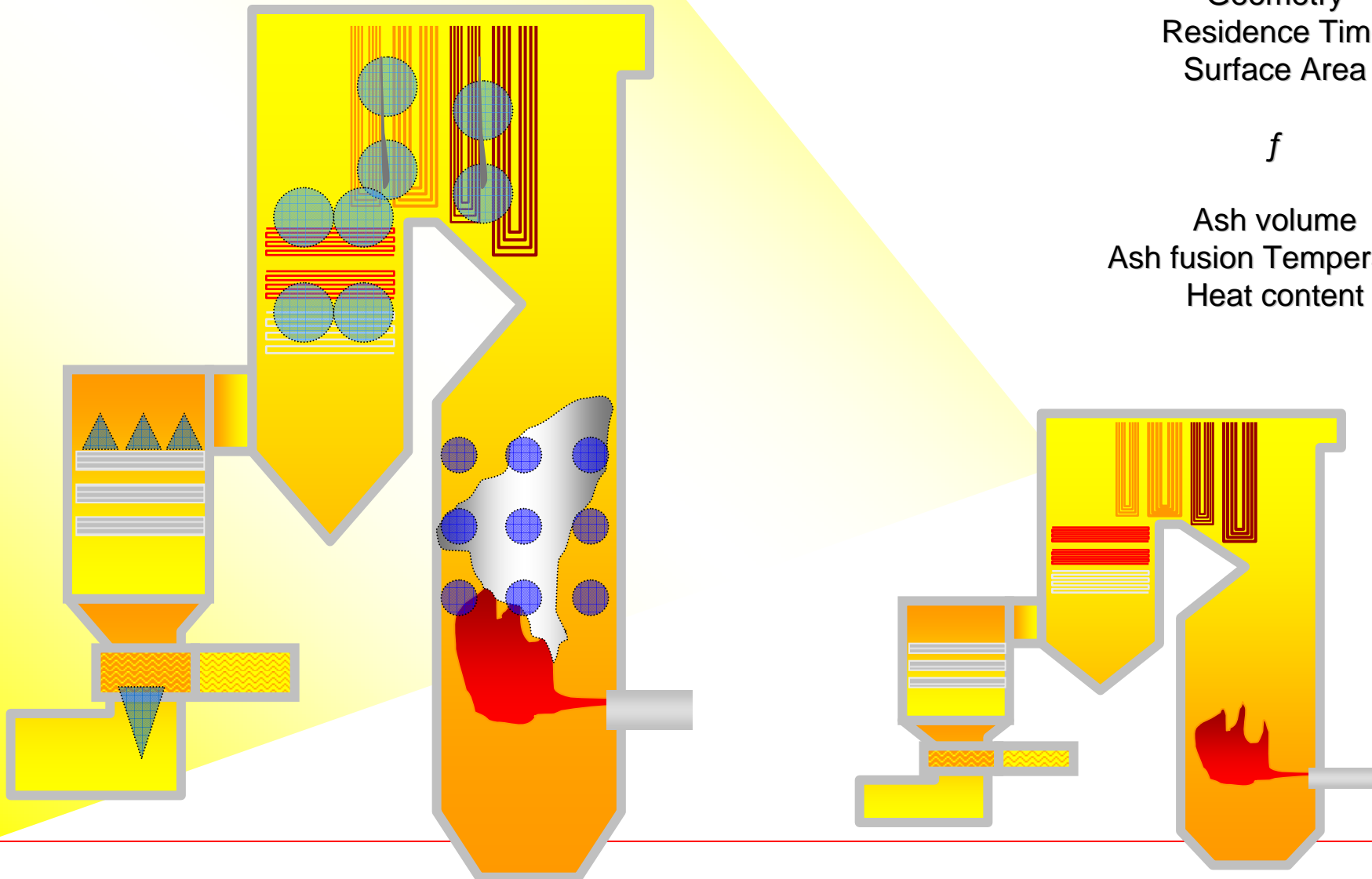
How the Ash Impacts the Boiler Design



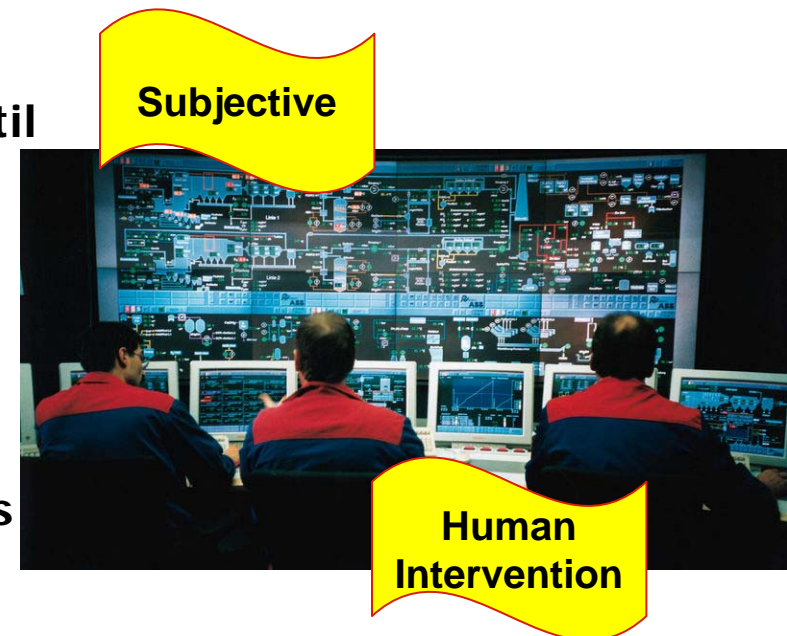
Geometry
Residence Time
Surface Area

f

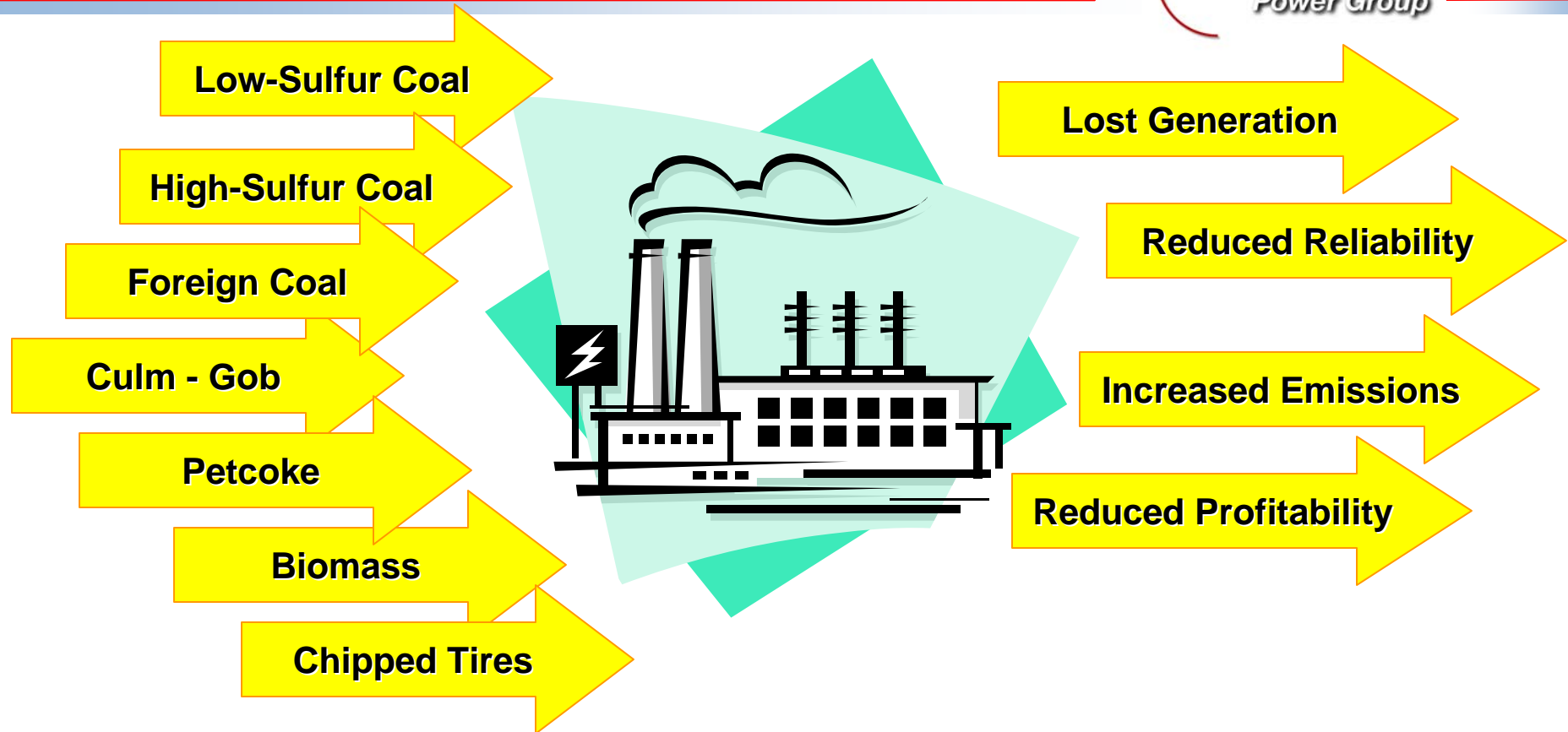
Ash volume
Ash fusion Temperature
Heat content



- Operators used global measurements to determine states of cleanliness in the various heat exchange sections
 - Operated various cleaning devices until such time as global measurements responded
 - ➔ Temperatures ?
 - ➔ ΔP
 - As the process was relatively stable operators developed fixed frequencies for individual and group sootblowing
 - These preprogrammed frequencies were programmed based on operator experience and judgment
 - ➔ Timing



Our Current Challenge - Fuel



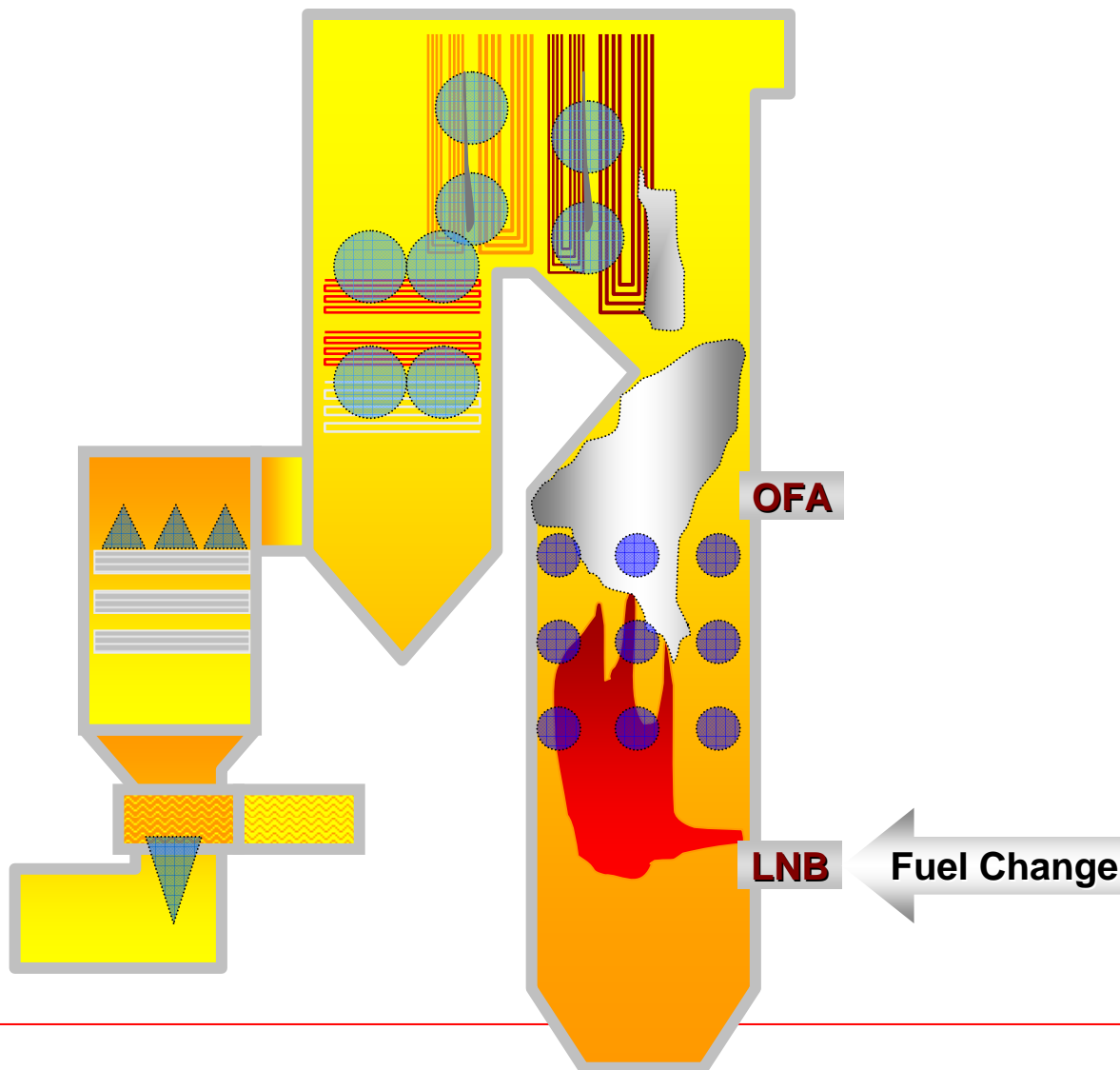
Current business conditions require a wide variety of compliance fuels to be burned

In a static boiler designed for a single fuel ...

With no detrimental impact on operations ...

And ... most also modified their combustion systems which exacerbates the problem...

We Have Changed the Operating Variables



If we change:

Ash volume
Ash fusion Temperature
Heat content

Via:

Fuel Changes
LNB / OFA

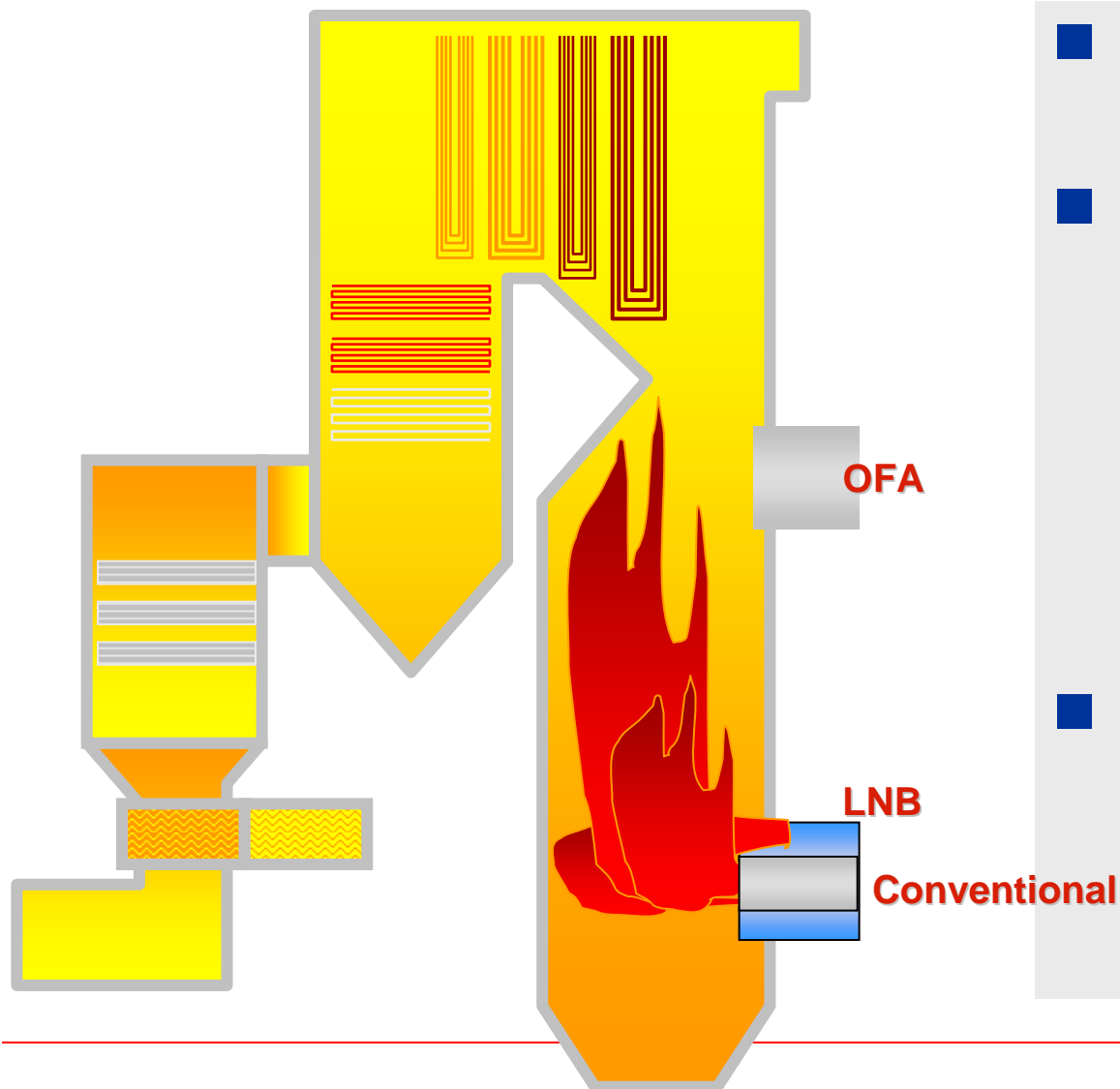
Without changing:

Geometry
Residence Time
Surface Area

- Ash deposition rates increase
- Location of deposits changes
- Ash tenacity increases

Sootblower System becomes ineffectual

- **Combustion modifications seek to reduce the amount of thermally created nitrous oxides by reducing combustion temperatures through staged combustion**
- **Low NOx Burners – LNB**
 - Stabilizes flame and increases mixing
 - Initiates partial combustion by creating a fuel-rich reducing atmosphere
 - Provides only 70% to 90% of required oxygen
 - Reduces NOx production by 30% to 55%
- **Over-Fire Air Ports – OFA**
 - Provides balance (10% to 30%) of required combustion air downstream of primary combustion
 - Combined with LNB may reduce total NOx production 40% to 60% even higher (70%) when gas re-burn technology is added



■ Effect on Cleanliness:

■ LNB

- Creates reducing atmosphere
- Reduces residence time
- Altered flame characteristics

■ OFA

- Moves transition zone close to convection surfaces

CHANGE - Varying Fuel Types



- **Economic and Legislative pressures are currently forcing the use of a wide variety of fuels that deviate from that which the boiler was designed to burn – Compliance Fuels**
- **Lo-Sulfur**
 - Typically sub-bituminous fuels burned in boilers designed for bituminous
 - Typically a loss in radiant heat transfer is experienced due to lower ash fusion temperatures
- **Hi-Sulfur**
 - Typically found in scrubbed units where economics dictate lower cost, higher sulfur fuels
 - Typically in conjunction with LNB/OFA, these fuels have a higher range of plasticity in a reducing atmosphere
 - With sulfur comes iron
 - Typically a loss in furnace heat transfer is experienced
- **Alternates**
 - Waste coal
 - Petcoke
 - Biomass, Tires, etc..

CHANGE - Varying Fuel Quality

Varying Fuel Quality



- Variations / Degradation in several coal quality metrics will have a substantial impact on slagging and fouling tendencies

■ Mineral Composition

- Quartz
- Pyrites

■ Chemical Composition

- Iron
- Alkalis
 - ➔ Calcium
 - ➔ Potassium
 - ➔ Sodium
 - ➔ Magnesium
- Silicates

+ or -

If you tune for + quality and get - quality = **UNDERCLEAN**

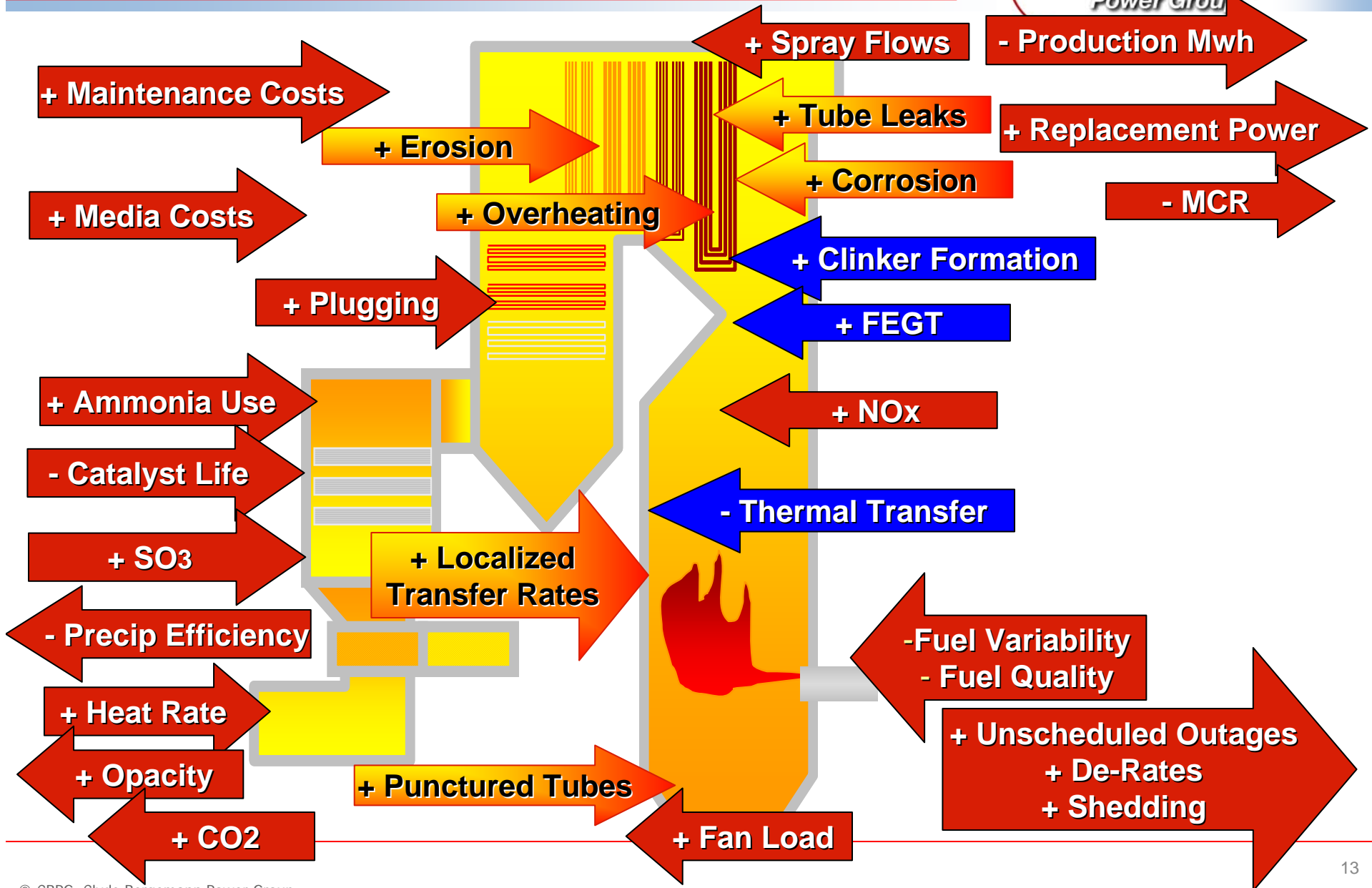
If you tune for - quality and get + quality = **OVERCLEAN**

Driving need for **DYNAMIC, Intelligent Cleaning System**

- **The operator's subjective cleaning cycles no longer working**
 - Over-Cleaning
 - Under-Cleaning
- **Culminating in lost generation**



Measurable Impact on the Process

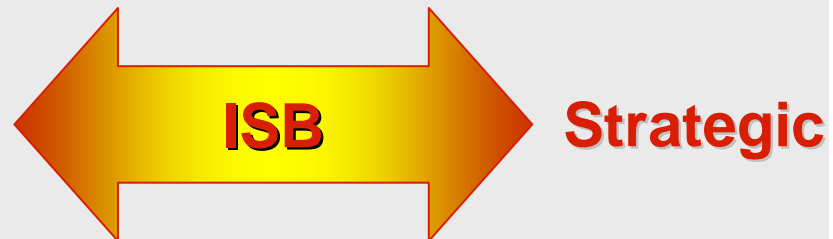


■ Reactive:

- Aggressive Over-Cleaning, increase frequency and intensity using only cleaning tools available
 - ➔ Tube leaks
 - ➔ Increased maintenance costs
 - ➔ Increased media consumption
- Load Shed & De-rate
- Off-Load blasting

■ Proactive

- Mill performance
- Combustion optimization
- Coatings
- Overlay
- MagOx
- SST Pendants



■ **EFFECTIVE SYSTEM DESIGN:**

- Matches the proper removal mechanism to the appropriate deposit type

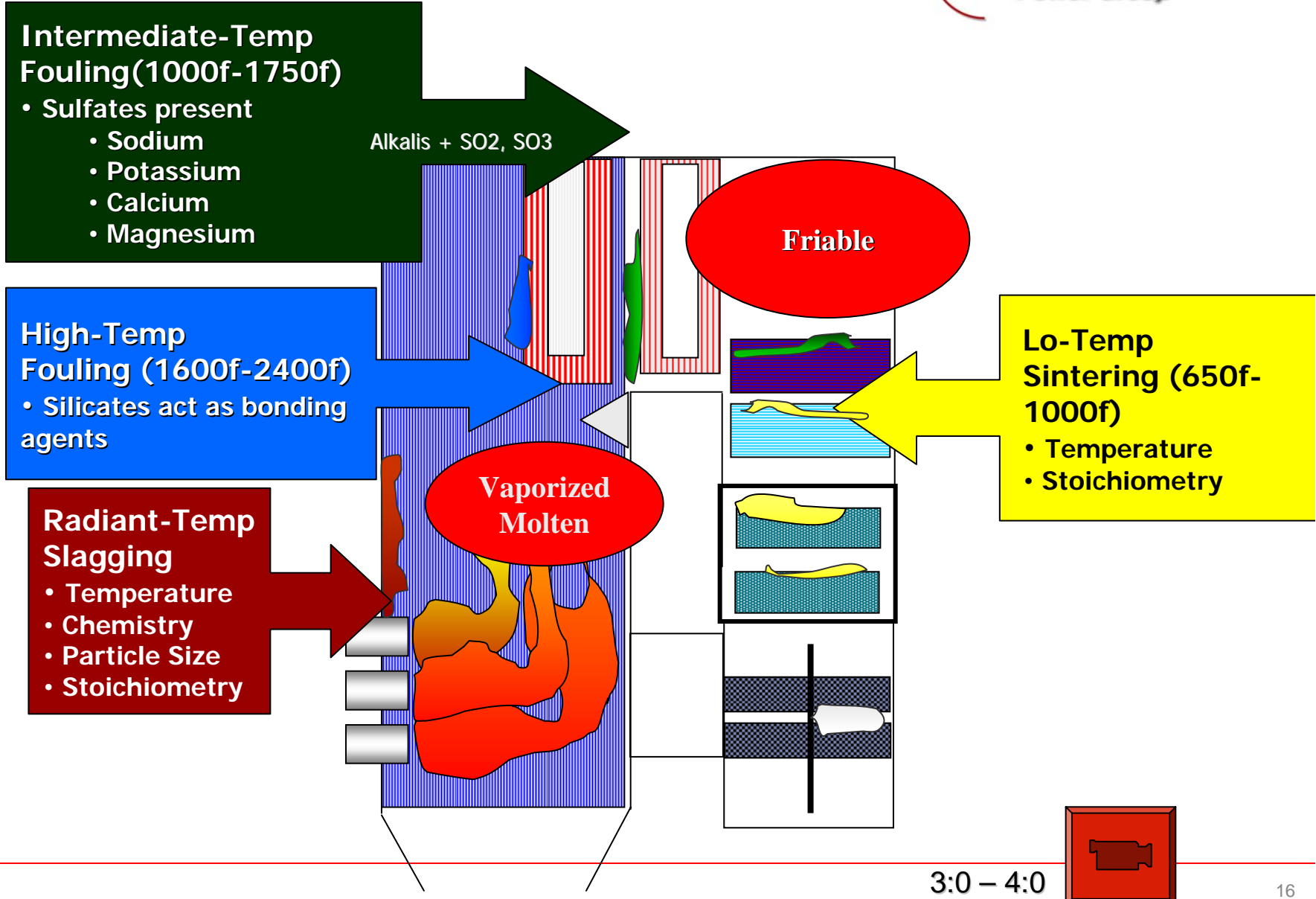
■ **CONVENTIONAL SYSTEM:**

- Initiates sequences
 - ⇒ Manually
 - ⇒ Preprogrammed frequencies

■ **INTELLIGENT SYSTEM:**

- Dynamically Initiates Cleaning Events:
 - ⇒ Only **WHEN** needed
 - ⇒ Only **WHERE** needed
 - ⇒ Using the proper medium **INTENSITY**

Classifying the Deposits

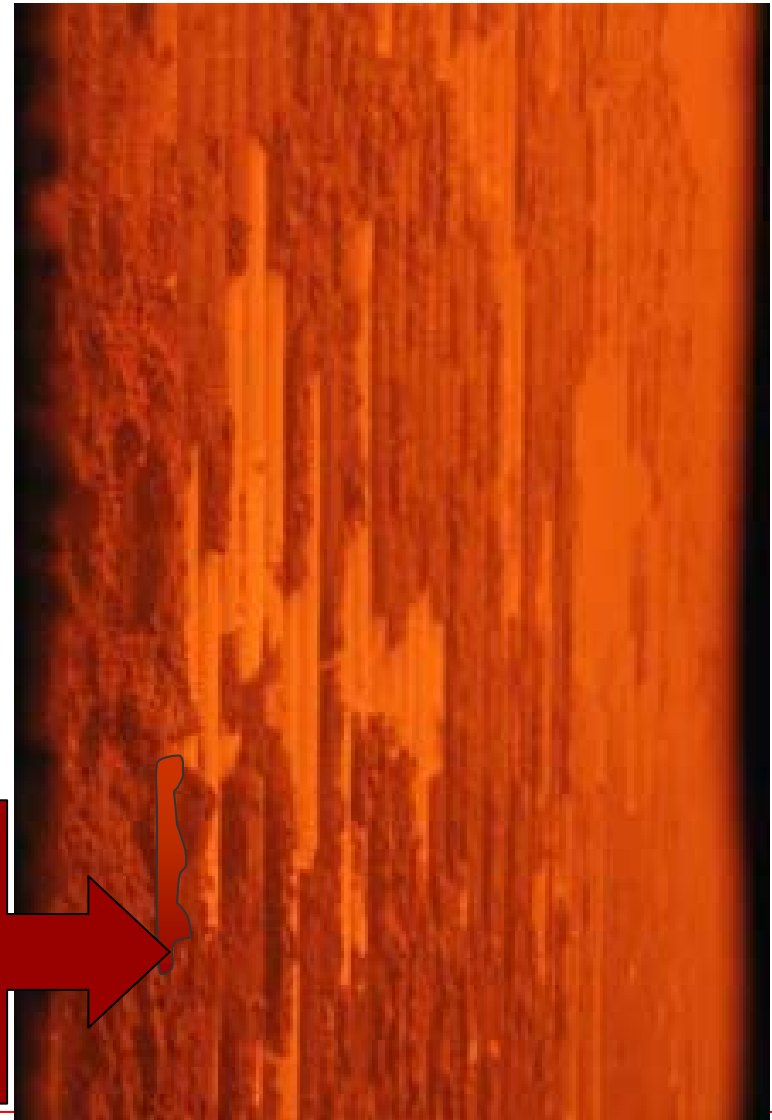


Furnace First !!!!!!!!!!!

- Furnace cleanliness sets the stage for cleanliness in the rest of the process
- Majority of heat release
- Be aware of the:
 - Deposit mechanisms
 - Principal heat transfer mechanisms

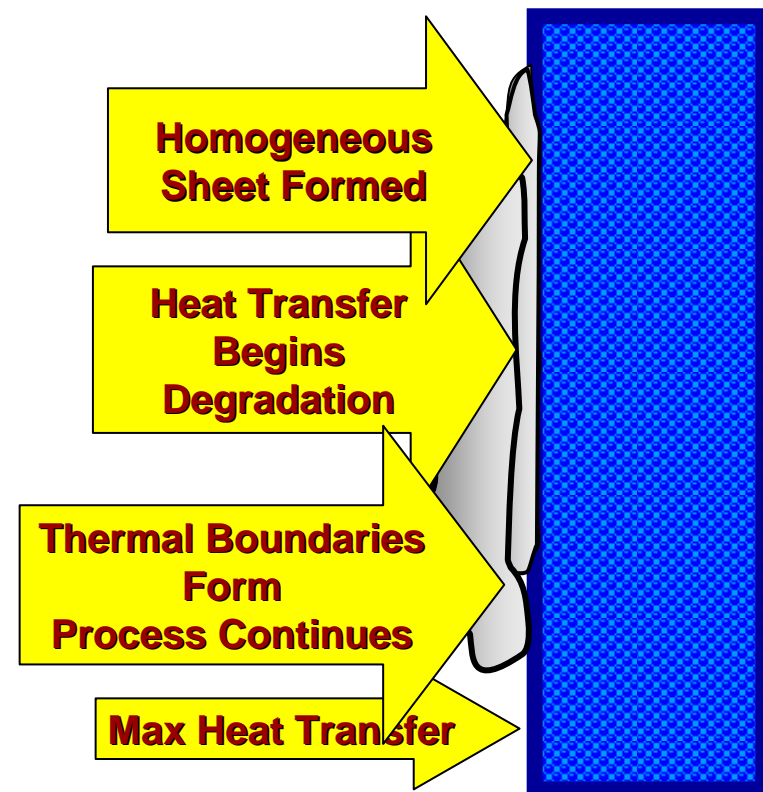
Radiant-Temp Slagging

- Temperature
- Particle Size
- Stoichiometry



A Closer Look at the Deposits

- With both mechanisms we see deposits form similarly:
 - Flight deposition causes small deposits to adhere to heat transfer surfaces
 - Deposits conjoin
 - Surfaces break down and begin to flow together
 - Groups of smaller deposits now form a homogeneous sheet
 - Subsequent flight deposits cause rapid increase in mass
 - Thermal boundaries form
 - Process continues



- Now that we know a bit about the cause of the problem and the types of ash deposits that we are faced with we will review the methods of on-load removal.
- **Ten Basic On-Load Ash Removal Mechanisms are currently available**
 - ➔ Hi-Impact – Impingement
 - ➔ Lo-Impact Impingement
 - Variable Dwell
 - Variable Helix
 - ➔ Lo-Impact Lateral
 - ➔ Hi-Impact Thermal
 - ➔ Lo-Impact Draft
 - ➔ Lo-Impact Acoustic
 - ➔ Lo-Impact Shockwave
 - ➔ Mechanical Vibration



■ Steam

- Most common due to availability of volume & pressure

■ Air

- Typically as effective as steam but supply volume & pressure typically not adequate or stable

■ Water

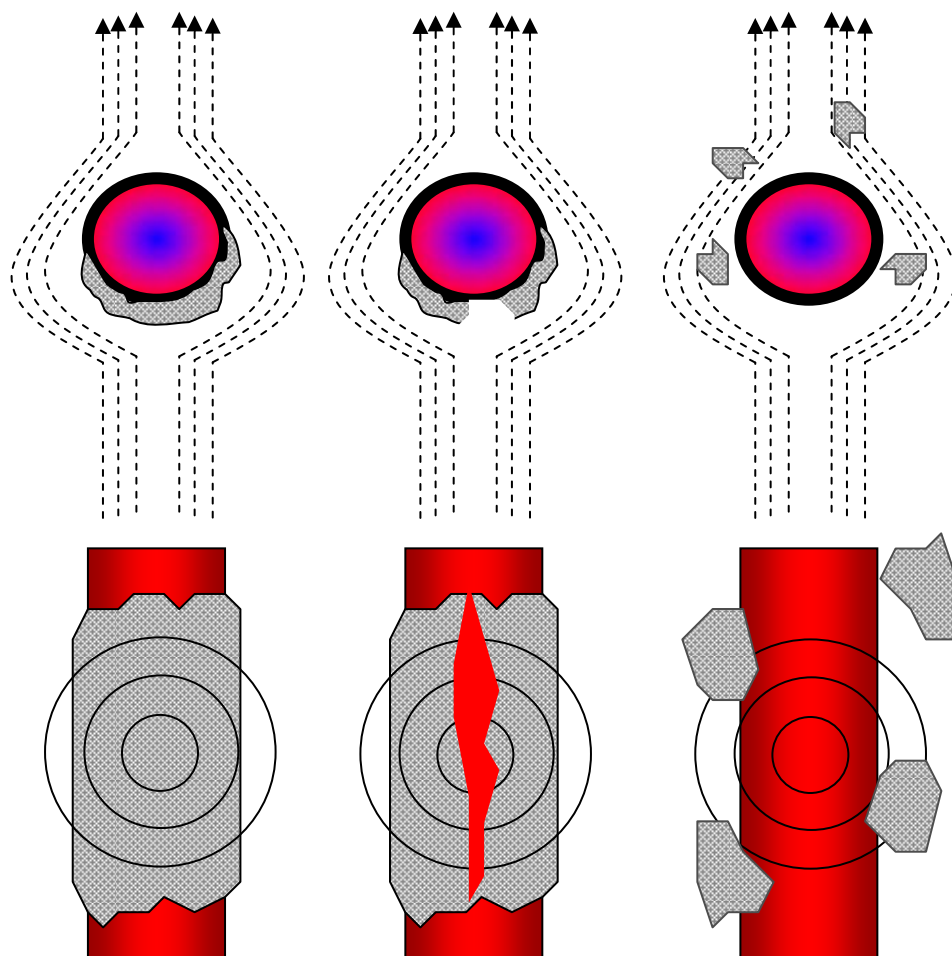
- Where deposits are expected to be in a plastic state

■ Sound

- Friable ash

■ Detonation

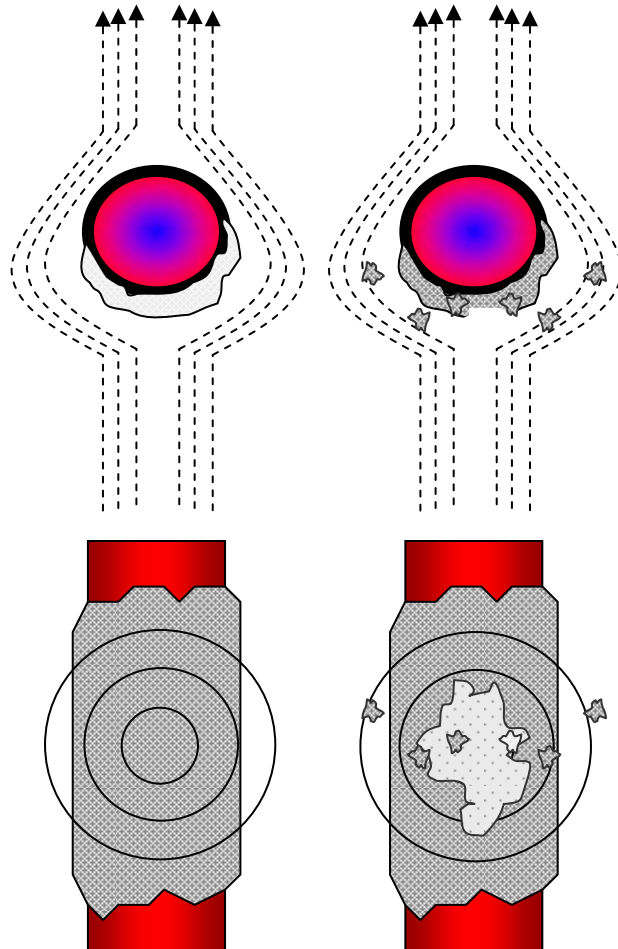
Hi-Impact - Impingement



Plasticity increases deposit strength

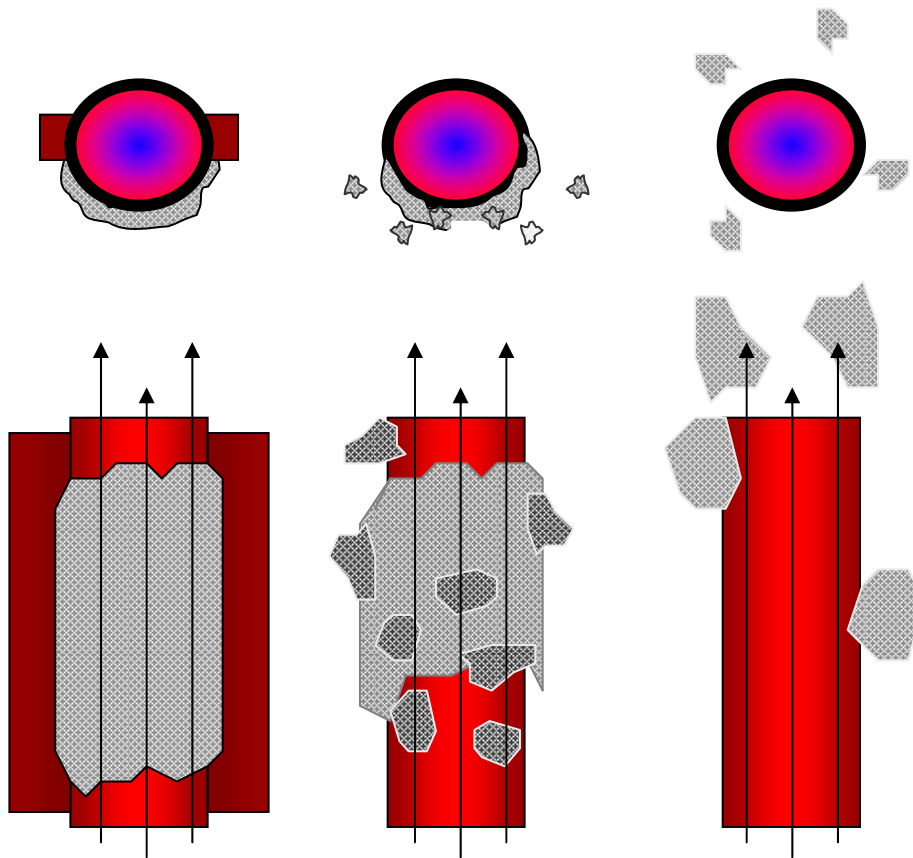
- Characteristic:
 - Direct Impingement
 - Impact pressure **exceeds** deposit strength
- Media impacts with high force
- Sets up laminar flow boundary – surface drag
- Circumferential shear forces create axial fissure
- Deposit instantaneously yields to:
 - High impact
 - Drag
- Single strike typically sufficient for removal

Lo-Impact - Impingement



Plasticity increases deposit strength

- Characteristic:
 - Direct Impingement
 - Impact pressure **less** than deposit strength
- Media impacts with low force
- Laminar flow & surface drag is insufficient to fracture deposit
- Surface of deposit begins to pit and erode
- Normal sootblower dwell times are insufficient to remove deposit
- Deposit requires:
 - **Longer dwell times**
 - **Multiple strikes**

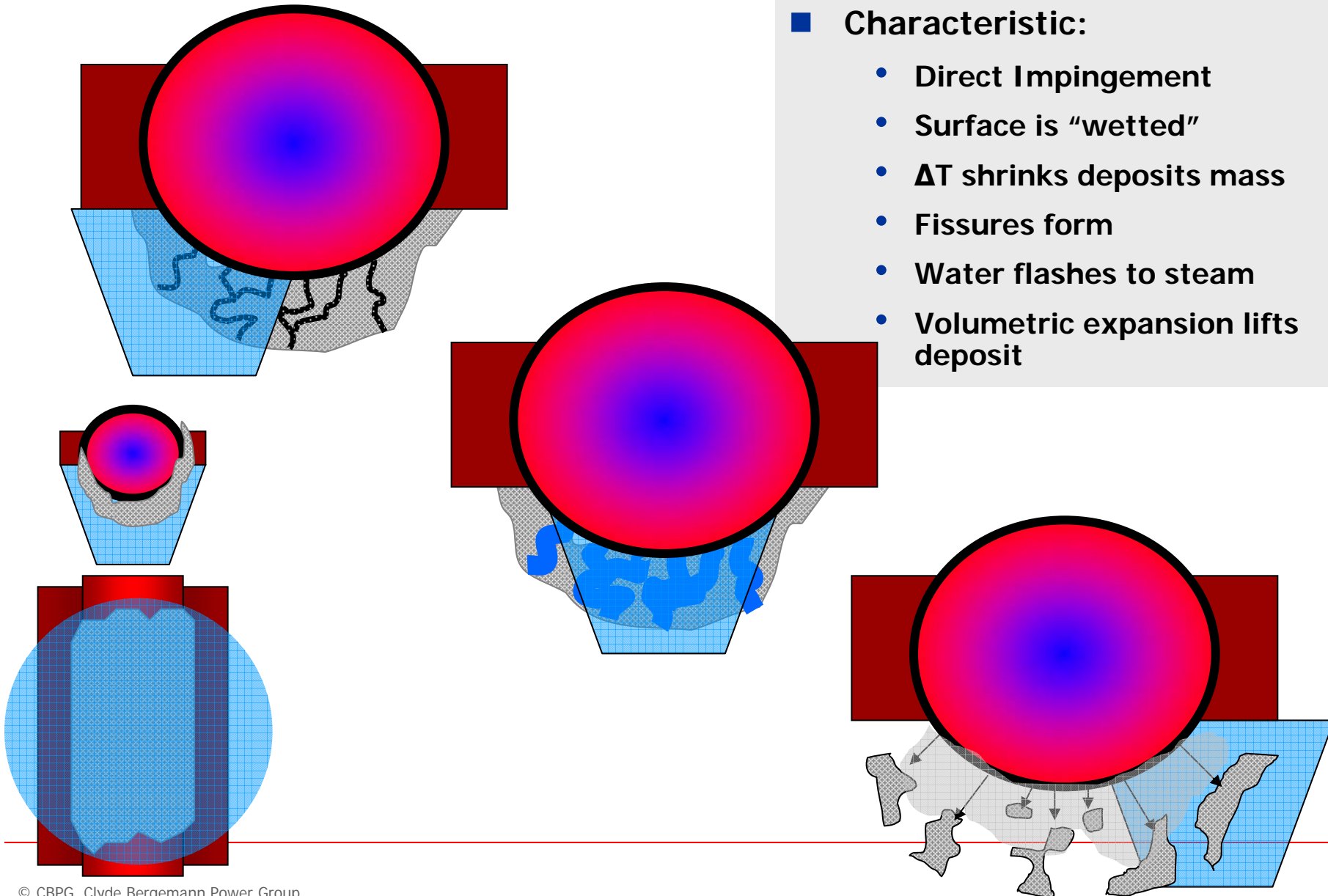


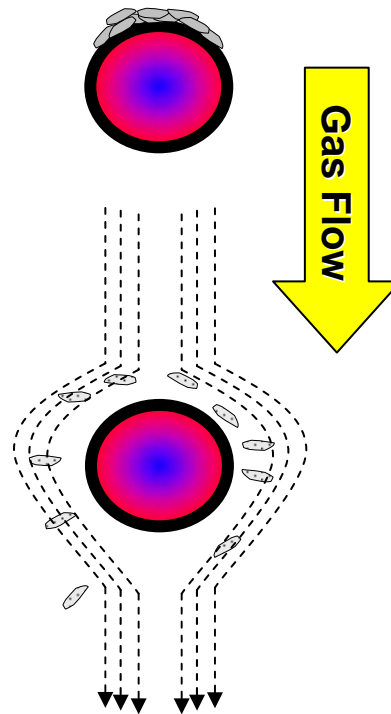
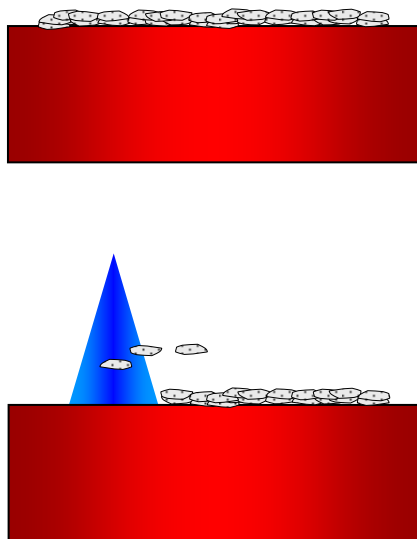
- Characteristic:
 - Parallel flow
- Media drags deposit with low force
- Impact pressure : deposit strength determines effective cleaning radius

Plasticity increases deposit strength and reduces cleaning radius sometimes to "0"

■ Characteristic:

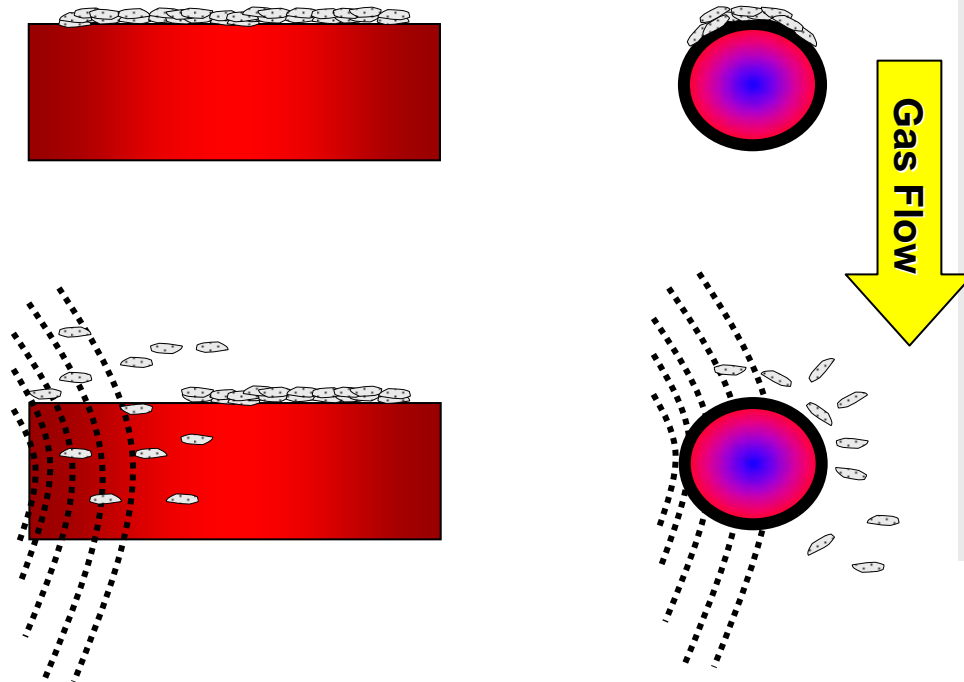
- Direct Impingement
- Surface is "wetted"
- ΔT shrinks deposits mass
- Fissures form
- Water flashes to steam
- Volumetric expansion lifts deposit





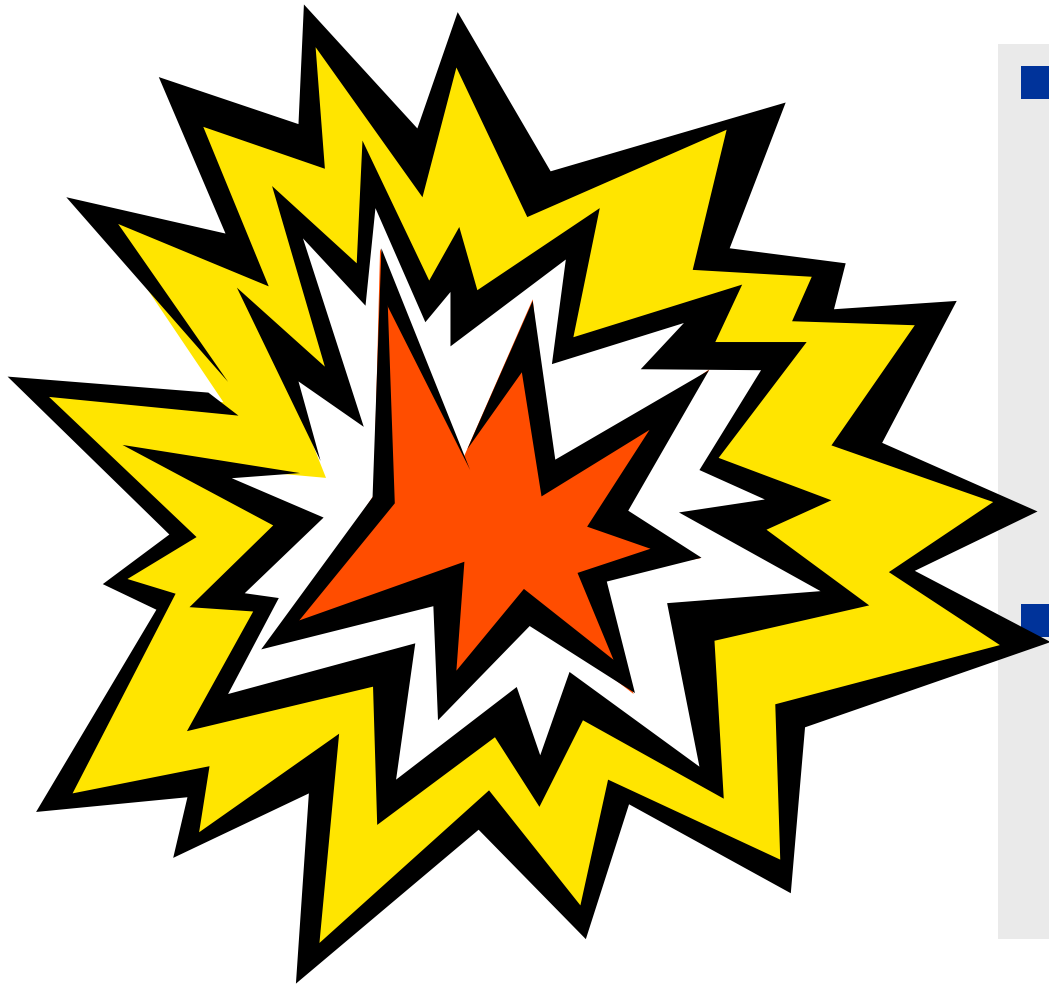
■ Characteristic:

- Ash not sintered into a cohesive deposit
- Adhesion and tensile strength low
- Drag of boundary layer sufficient to dislodge deposit
- Low impact pressure "dusting" with steam or air maintains surface cleanliness
- Relies principally on flow through open annulus area as opposed to direct impingement



■ Characteristic:

- Ash not sintered into a cohesive deposit
- Adhesion and tensile strength low
- Frequent low impact acoustic “dusting” maintains surface cleanliness if:
 - Moisture not present
 - Sufficient air pressure available to sonic cleaners
 - Maldistribution not an issue



■ Characteristic:

- Rapid expansion of detonated gases creates shockwave
- Wave propagates throughout cavity to dislodge ash particles from surface

■ Form

- Off-load explosives
- Propane driven detonation device

- As opposed to sonic & pulse which vibrate the atmosphere rapping vibrates the heat exchange surface through direct & intermittent mechanical force
- Two basic technologies:
 - Tumbling hammers
 - Piston

Evolution of Cleaning Tools



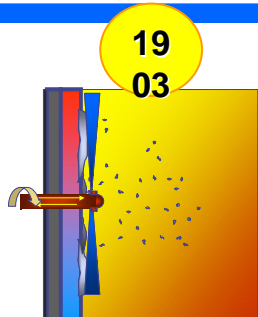
RETRACTABLE

- Fixed Helix
- Fixed Media
- Subjective Actuation



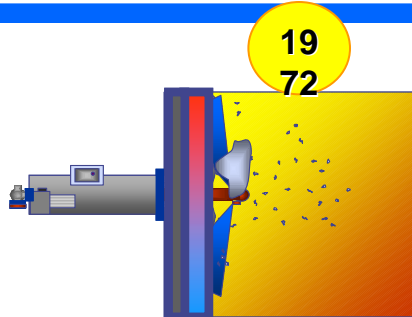
SMART Retractable

- Variable Helix
- Open-Loop Control or Full Closed-Loop Control



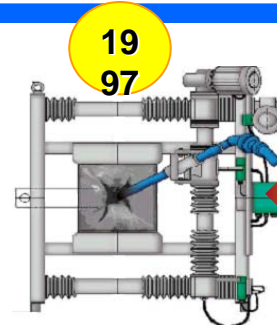
WALLBLOWER

- Parallel Cleaning Jet
- Subjective Actuation



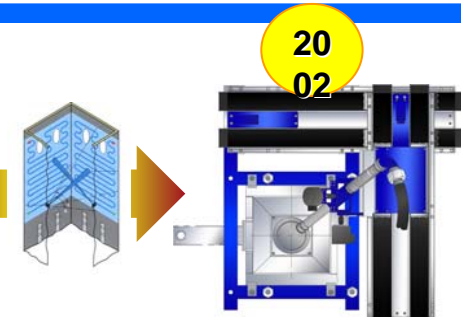
WATER LANCE

- Back-raked Cleaning Jet
- Subjective Actuation



WATER CANNON

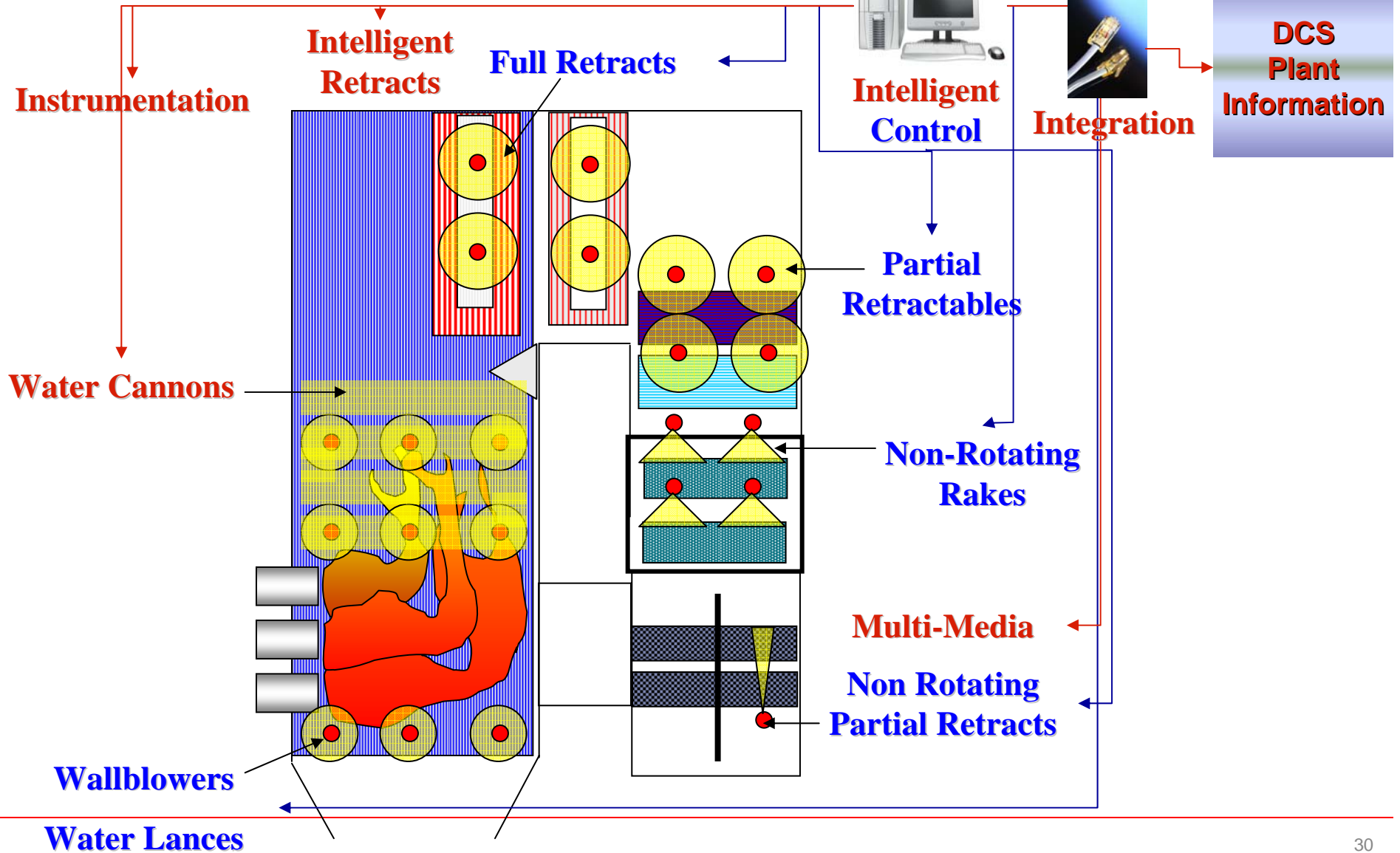
- Opposed Wall Cleaning Jet
- Intelligent Actuated



SMART CANNON

- Opposed Wall Cleaning Jet
- Full Closed-Loop Actuation

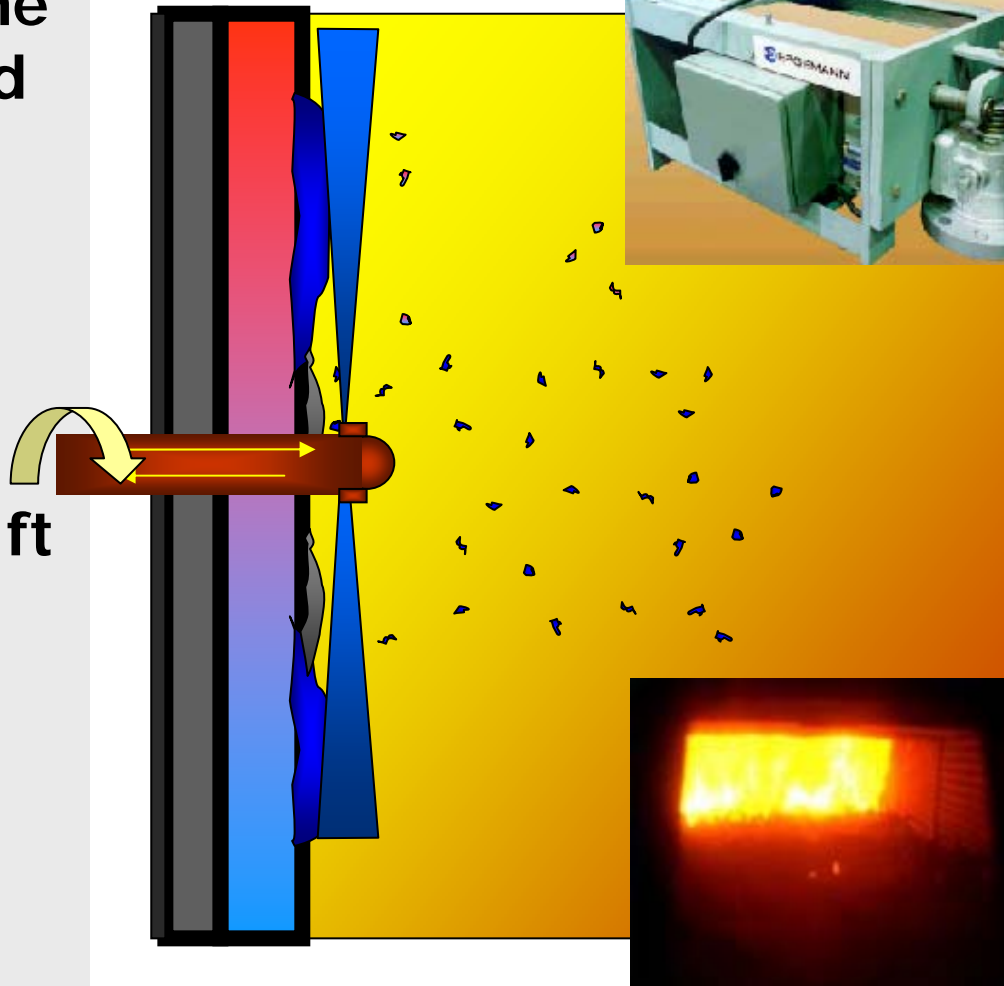
Sootblower System Overview



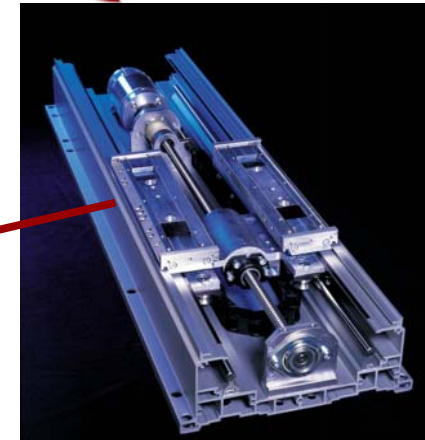
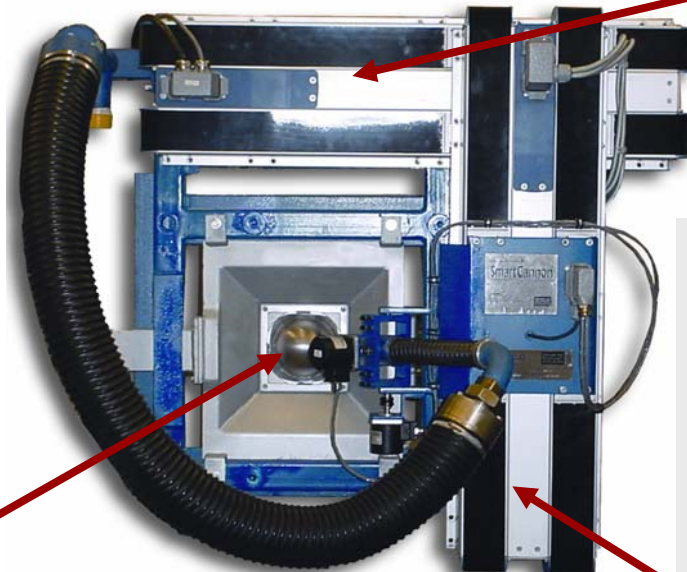
Traditional Furnace Cleaning



- Traditional Radiant Zone Cleaning utilized a fixed cleaning device which positions a steam / air cleaning jet parallel to the water wall tube
- Affected areas range from 28 sq ft to 115 sq ft depending on deposit strength
- Limited treatment of < 20% of critical surface area

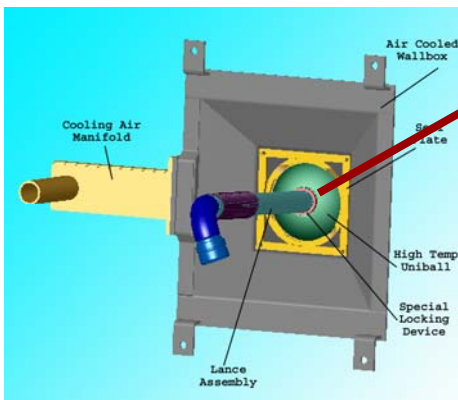
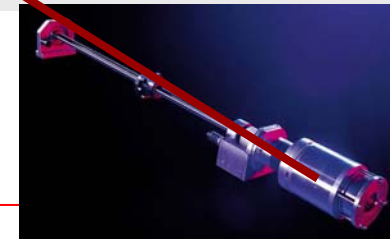


SmartCannon® Reliable - Accurate



Sealed Linear Screw Drives

- 24V Brushless DC Servo Motors
- Gear Reducer
- Linear Drives
- Ball Caster Spindle
- Magnetic Sealing

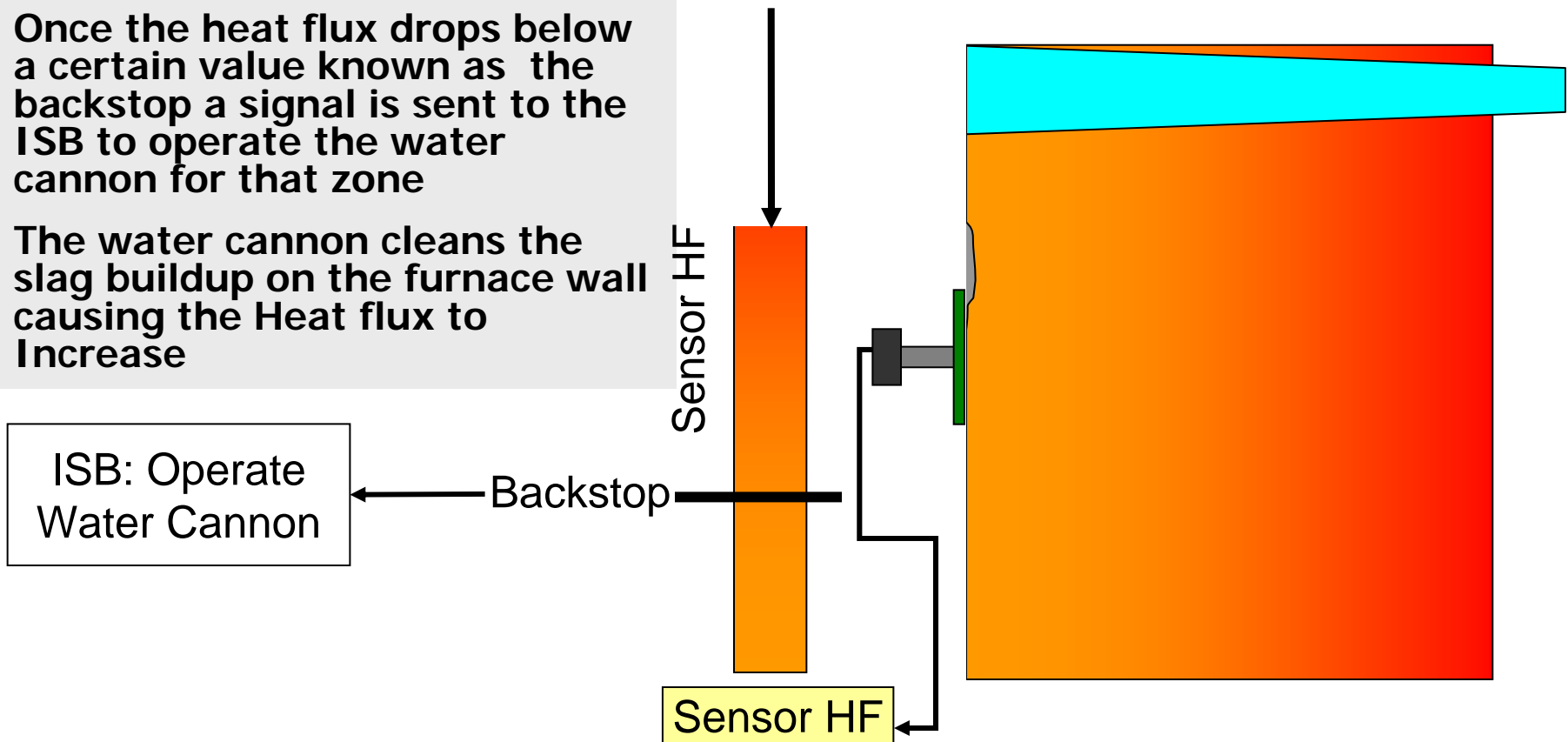


- Positive Seal Wallbox
- Uni-Ball Construction

Smart Furnace: Heat Flux Sensors

- When slag begins to build up on the furnace walls the measured heat flux starts to decrease
- Once the heat flux drops below a certain value known as the backstop a signal is sent to the ISB to operate the water cannon for that zone
- The water cannon cleans the slag buildup on the furnace wall causing the Heat flux to Increase

Calculate Thermal Impact

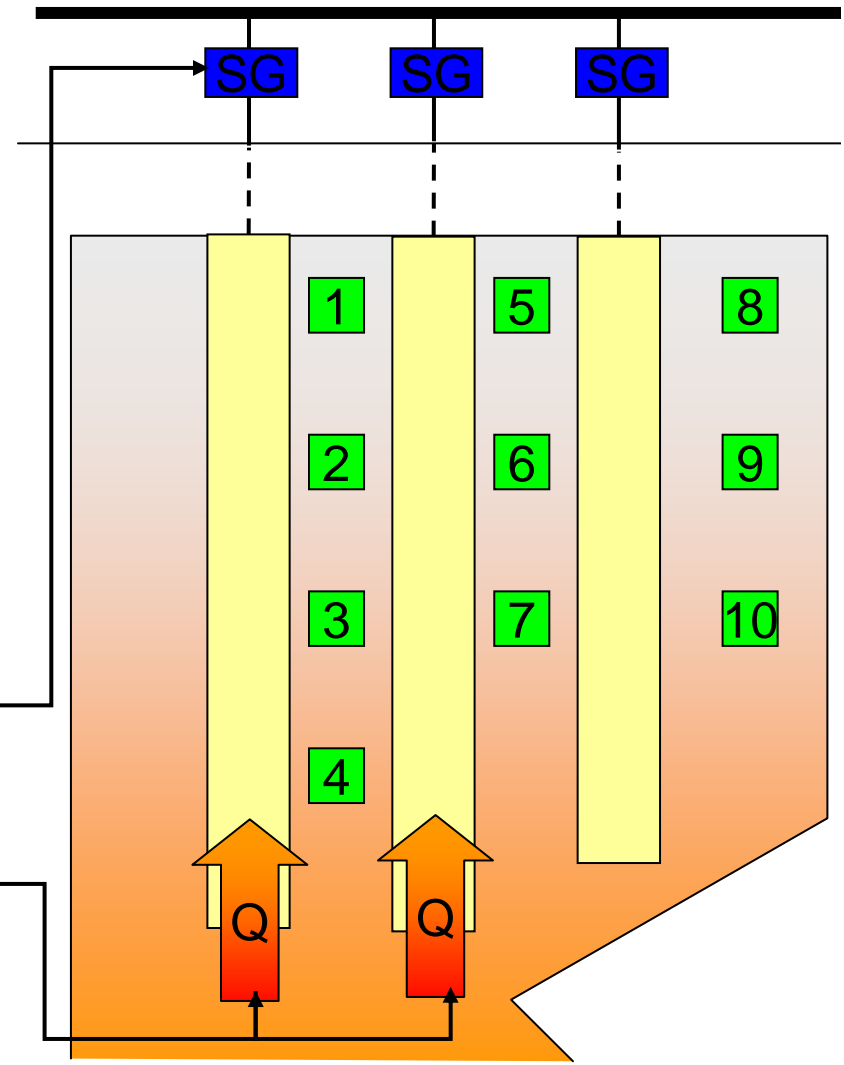


Smart Convection

- **SuperHeater Fouling Monitor:**
 - Determines Boiler cleanliness from Strain Gauges mounted to the Hanger Rods
- **ThermoDynamic Model**
 - Determines Boiler Cleanliness from calculating the Heat Transferred into each heat exchanger

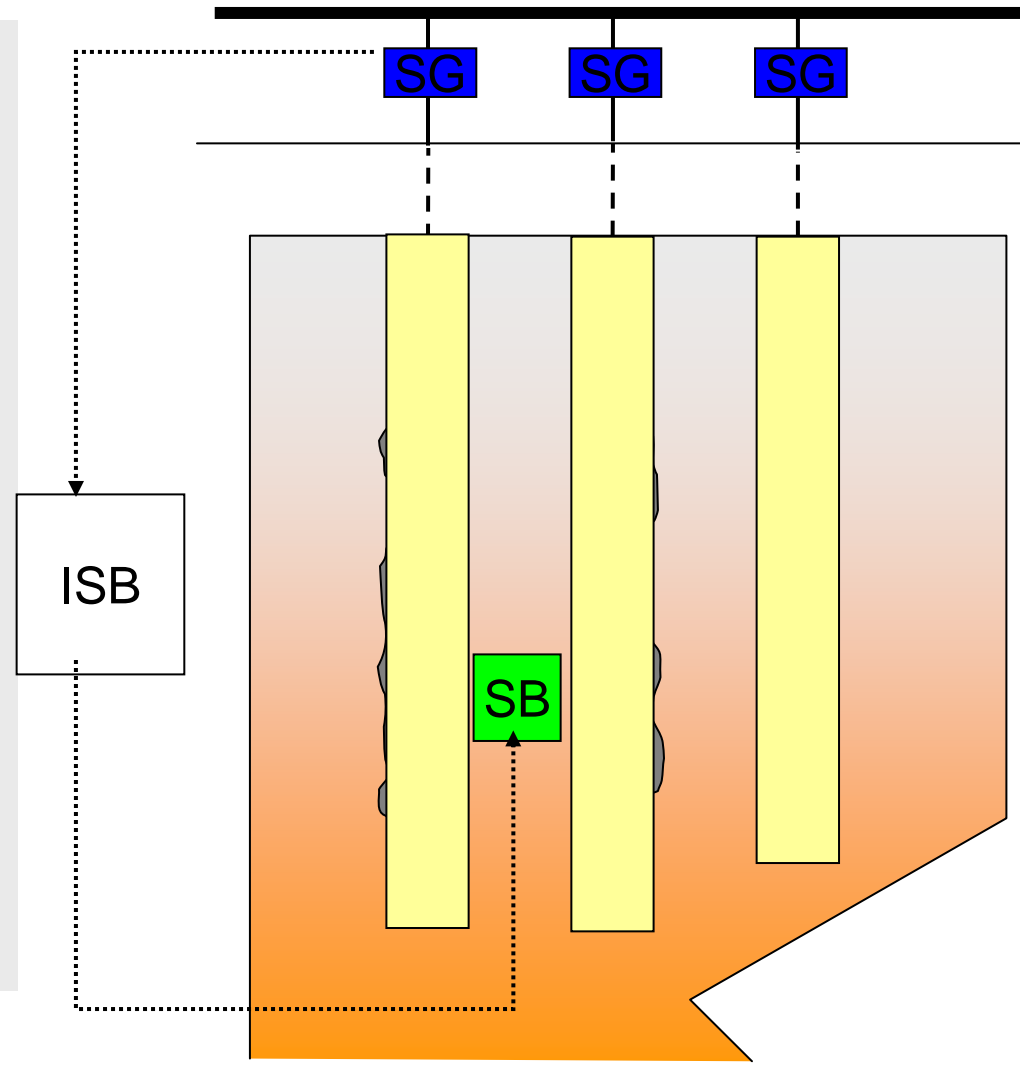
SuperHeater
Fouling Monitor

ThermoDynamic
Model



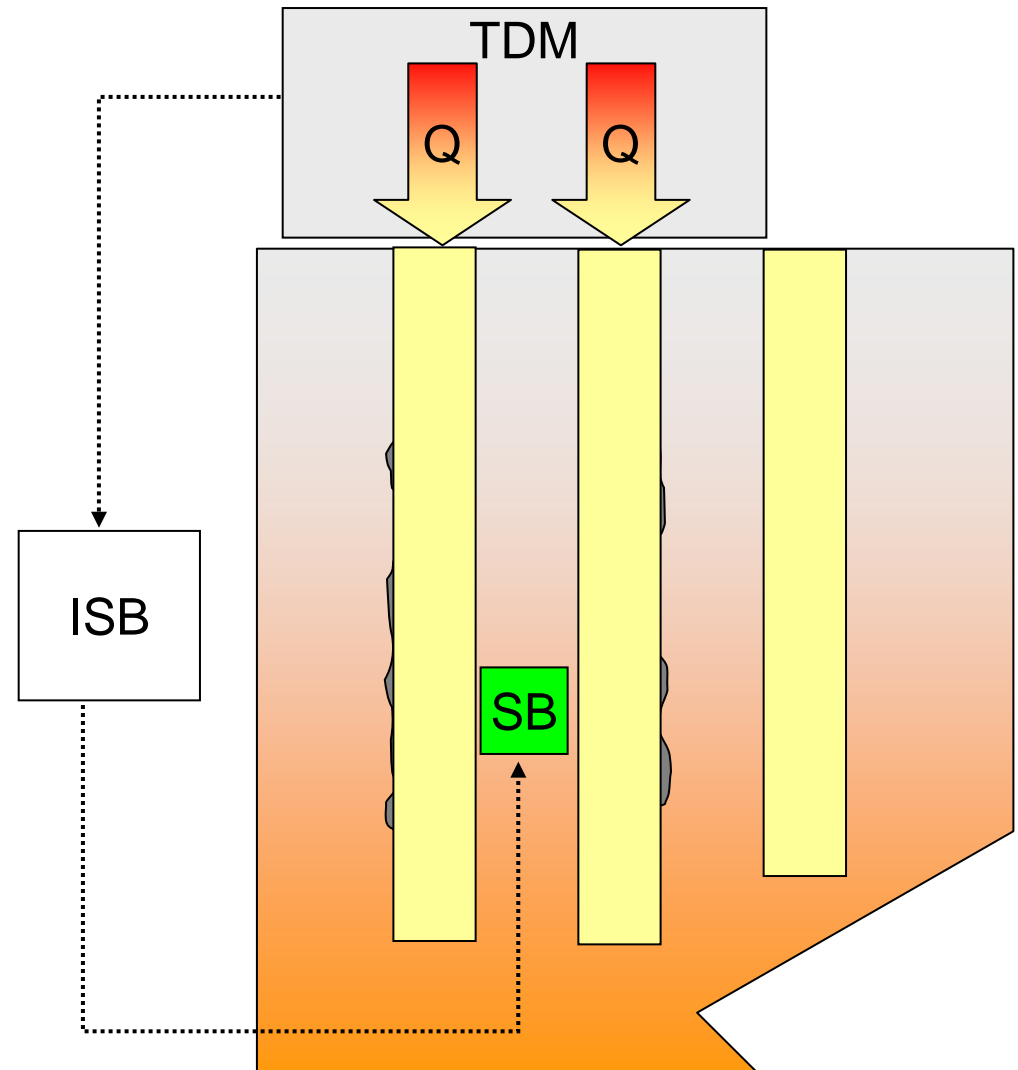
SuperHeater Fouling Monitor

- **Monitors Weight Accumulation on pendants**
- **As deposits stick to the tube banks the overall weight of the tube bank increases**
- **This increase in weight is detected by the Smart Gauges located on the hanger rods**
- **The strain gauges relay the increase in weight to the ISB system**
- **The ISB system then operates the correct sootblower to remove the deposit**

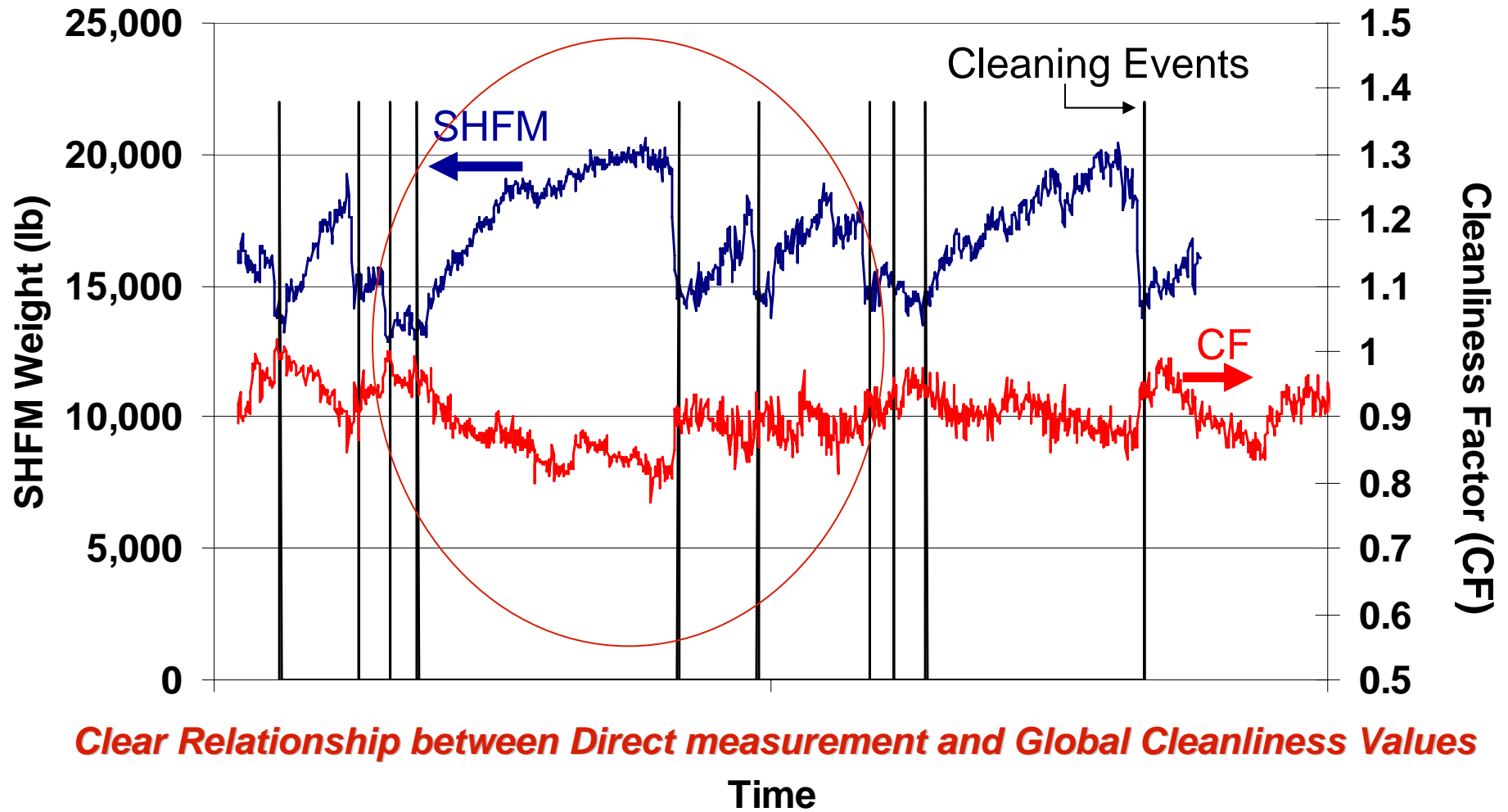


ThermoDynamic Model

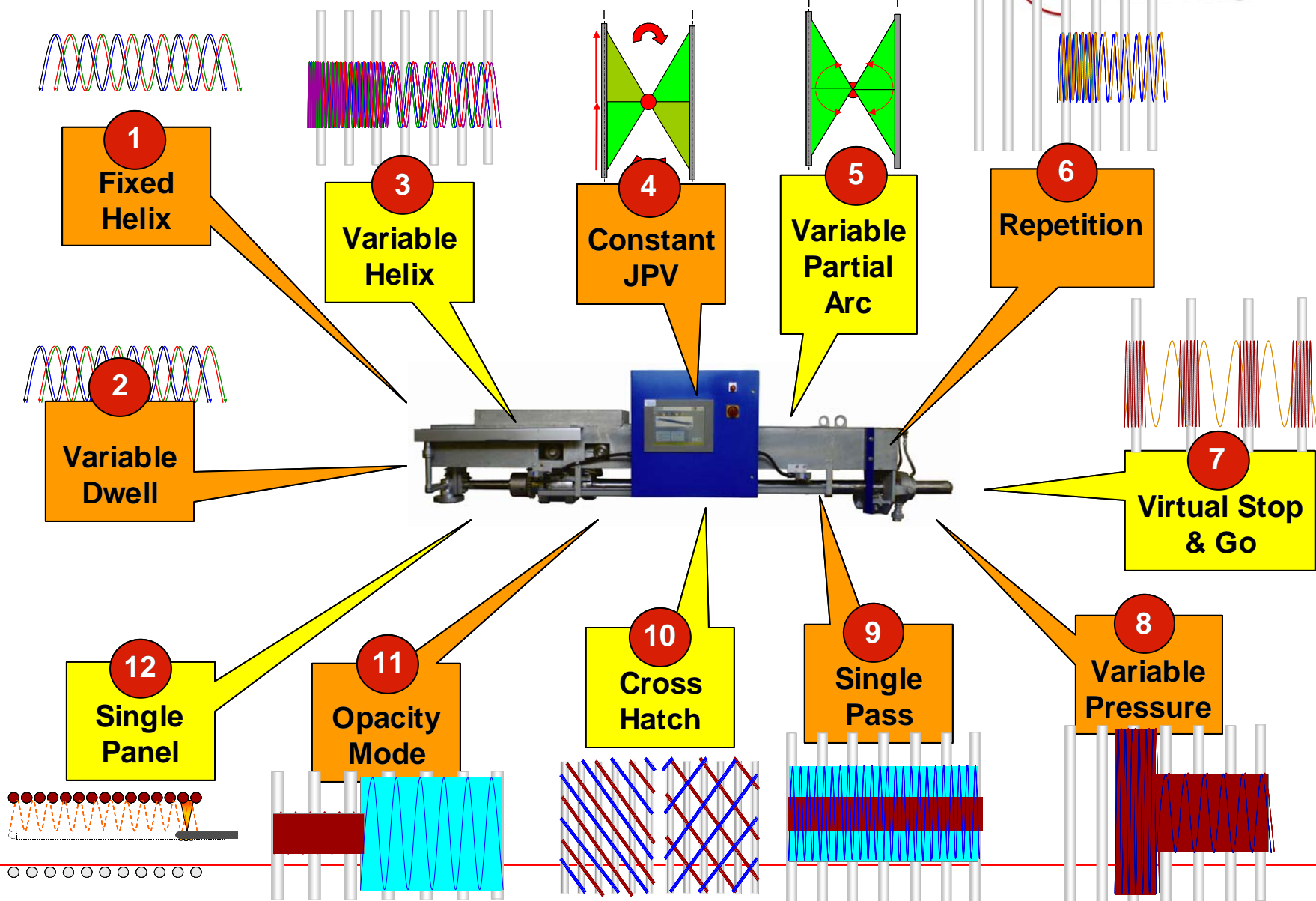
- Monitors Inlet and Exit Temperatures and Flows for each heat exchanger
- As deposits stick to the tube banks the overall heat transferred (Q) to the tube banks decreases
- This decrease in heat transfer is detected by the Thermodynamic model
- The TDM relays the decrease in heat transfer to the ISB system
- The ISB system then operates the correct sootblower to remove the deposit



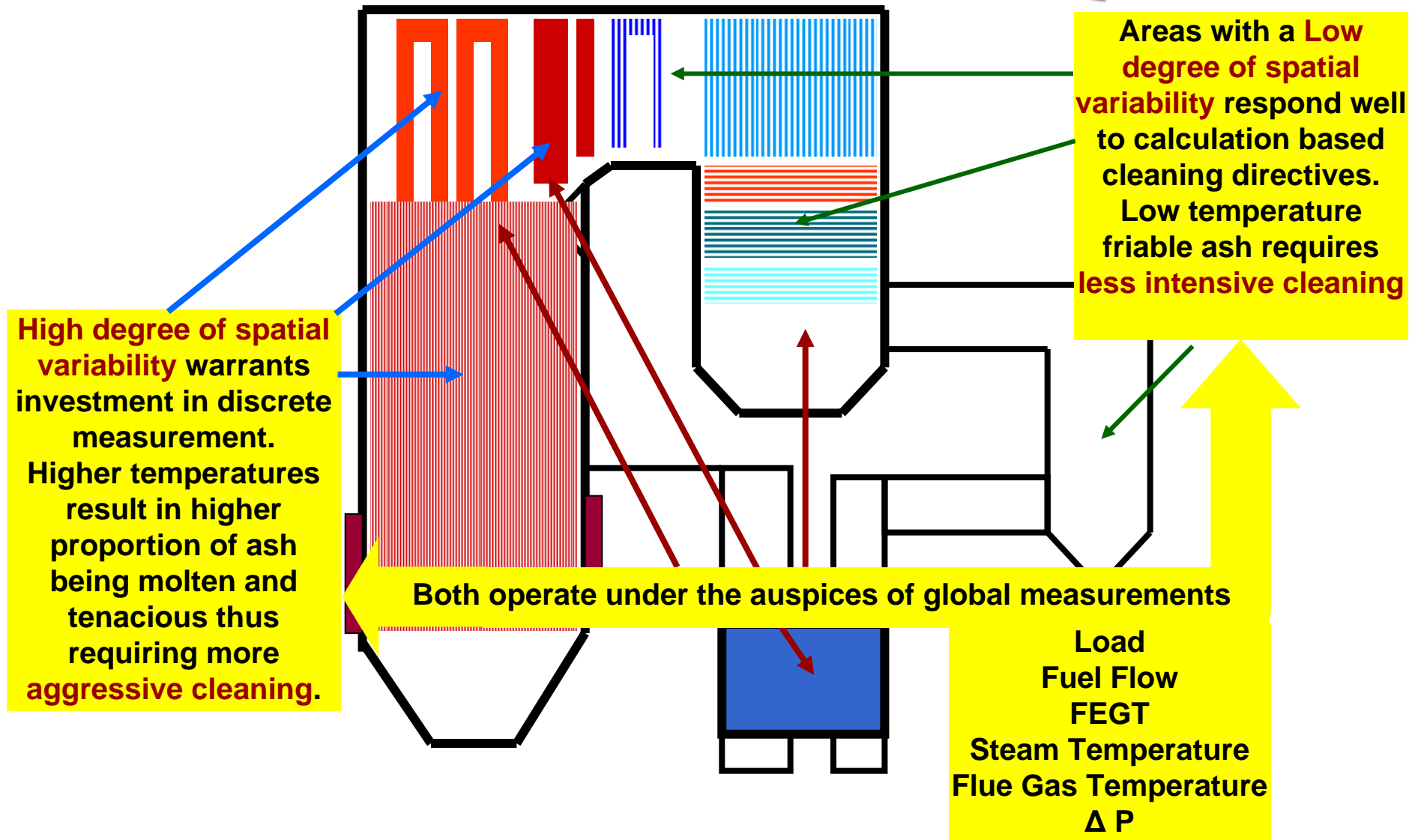
LCRA U1 - Superheater Pendant



Tools – Smart Retractable Cleaners



When to Instrument - Global:Discrete





SmartGauge

Monitors pendant ash accumulations to intelligently guide sootblower operation



SmartVision

Developmental system providing analog and digital mapping of hidden ash deposits



Infrared Imaging

Provides operators with visual confirmation of instrument output relative to current slagging and fouling conditions



Pyrometer

Pyrometry provides accurate FEGT to serve as a background permissive



SmartSensor

Monitoring heat flux and thermal impact simultaneously to guide cannon operation



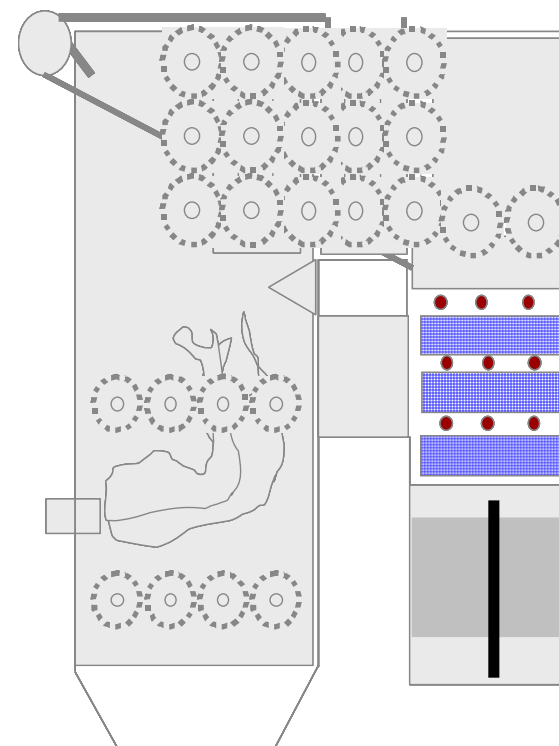
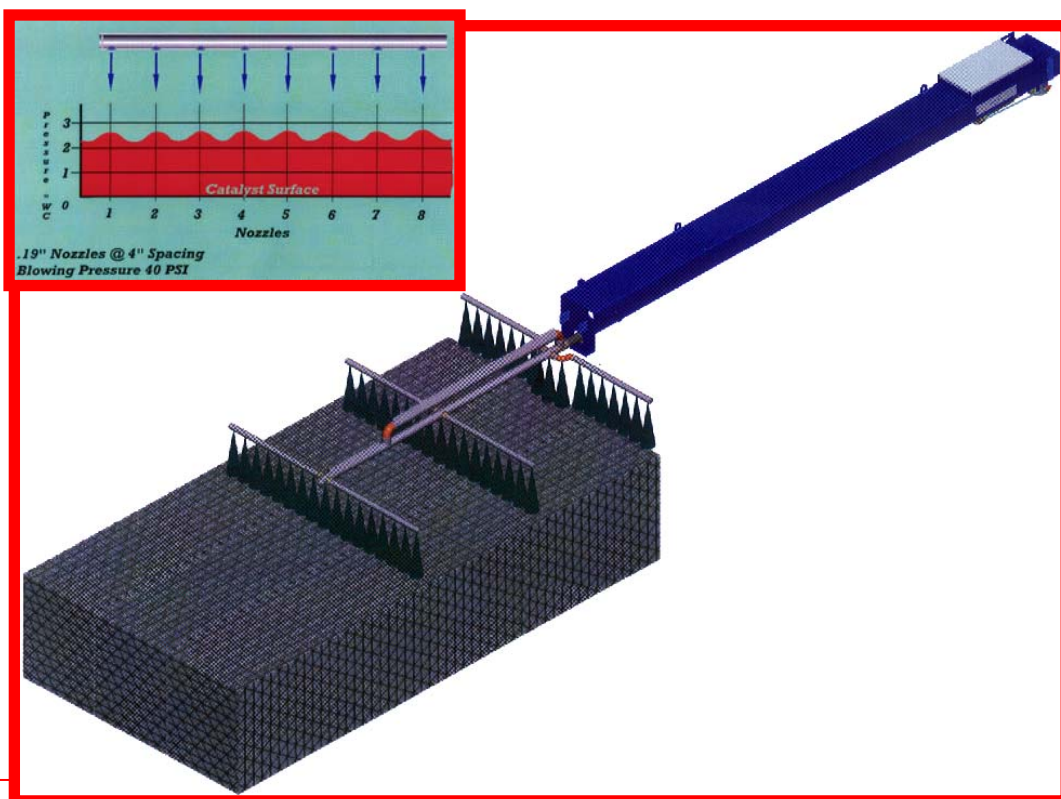
Membrane Sensor

Provides positive feedback on Cannon impact accuracy

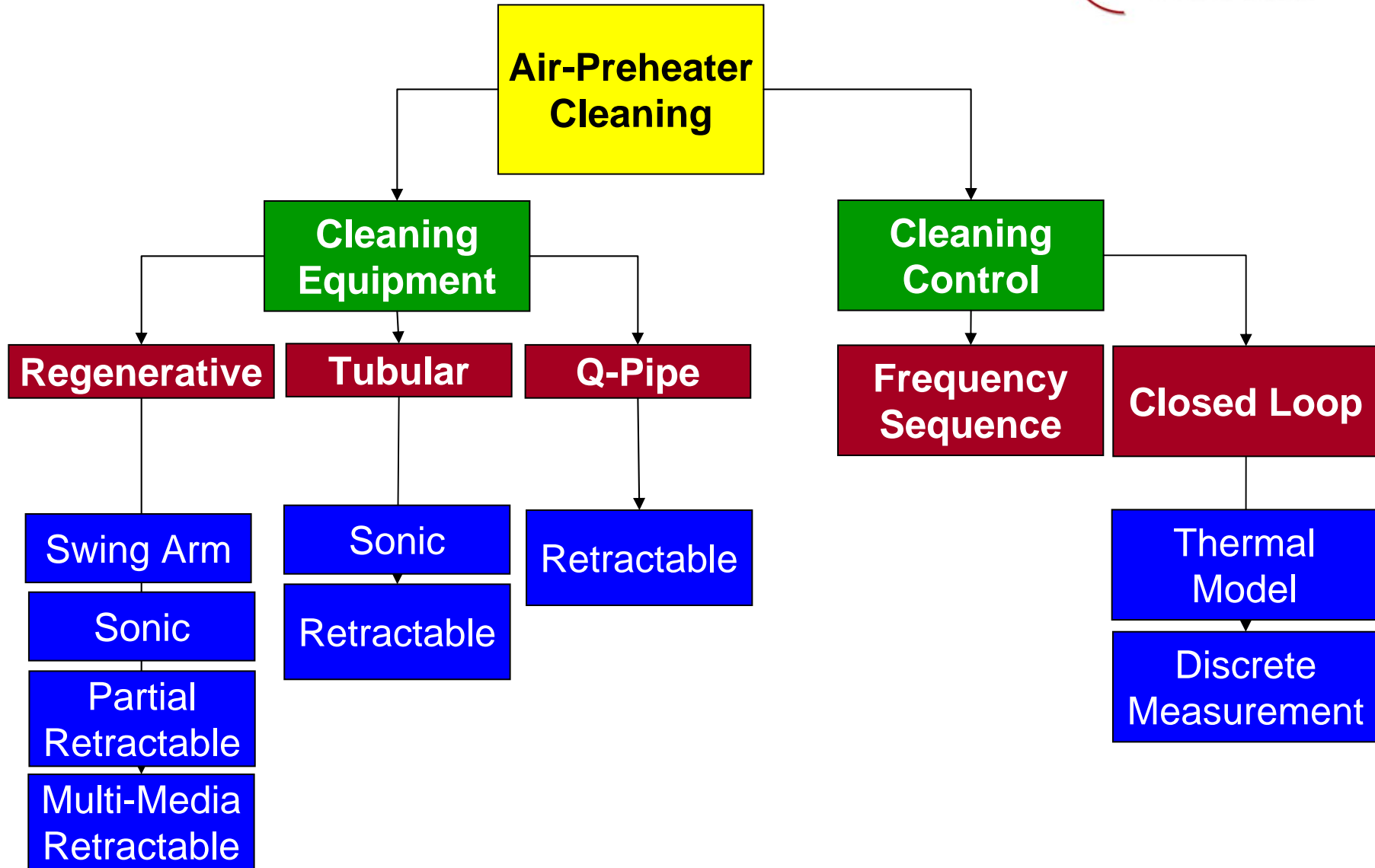
SCR Cleaning

■ Non-rotating variant of the US Retractable

- Appendages with nozzles on 4" centers clean entire surface

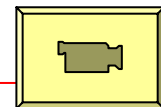
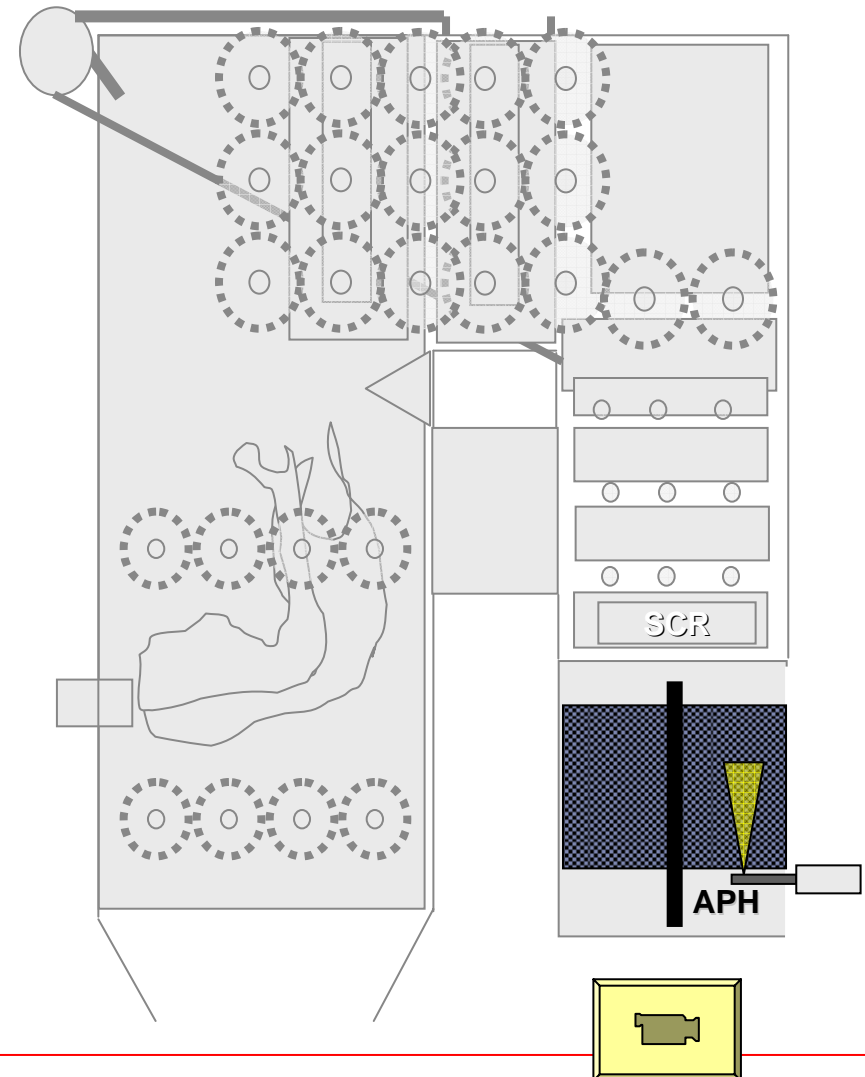
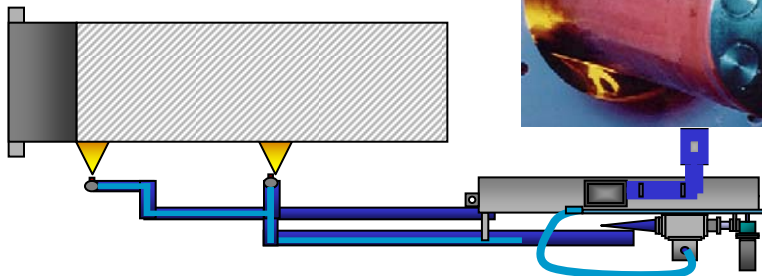
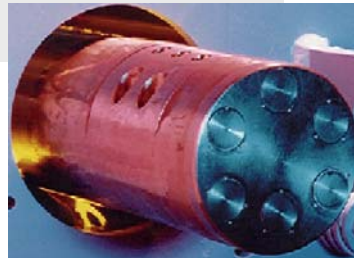


Air-Preheater Cleaning

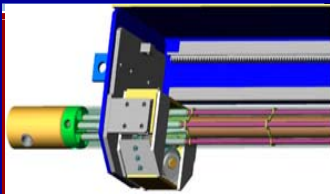


APH Cleaning

- With the advent of the SCR and potential ammonia bisulphate deposits integral water wash capabilities have become increasingly important
- Multi-Media APH cleaners are fully programmable to vary dwell time and step size for both steam and water cleaning



Cleaning Tools



SmartLance
The ultimate in retractable cleaner technology offering both Multi-Mode and Multi-Media flexibility

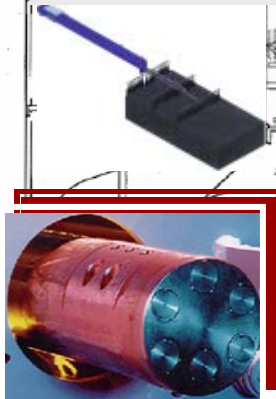


SmartUS
Eliminates the constraints of traditional retractables by providing the world's only full-feature retractable

Rake Cleaners
Proven effective safe SCR Catalyst Cleaning



US/USX
Severe-Duty single motor drive retractable sootblower platform



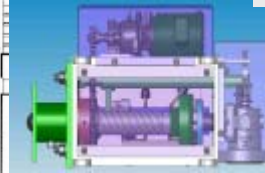
APH Cleaner
Multi-Media Air Preheater cleaner alternates between normal steam cleaner and high-pressure washing



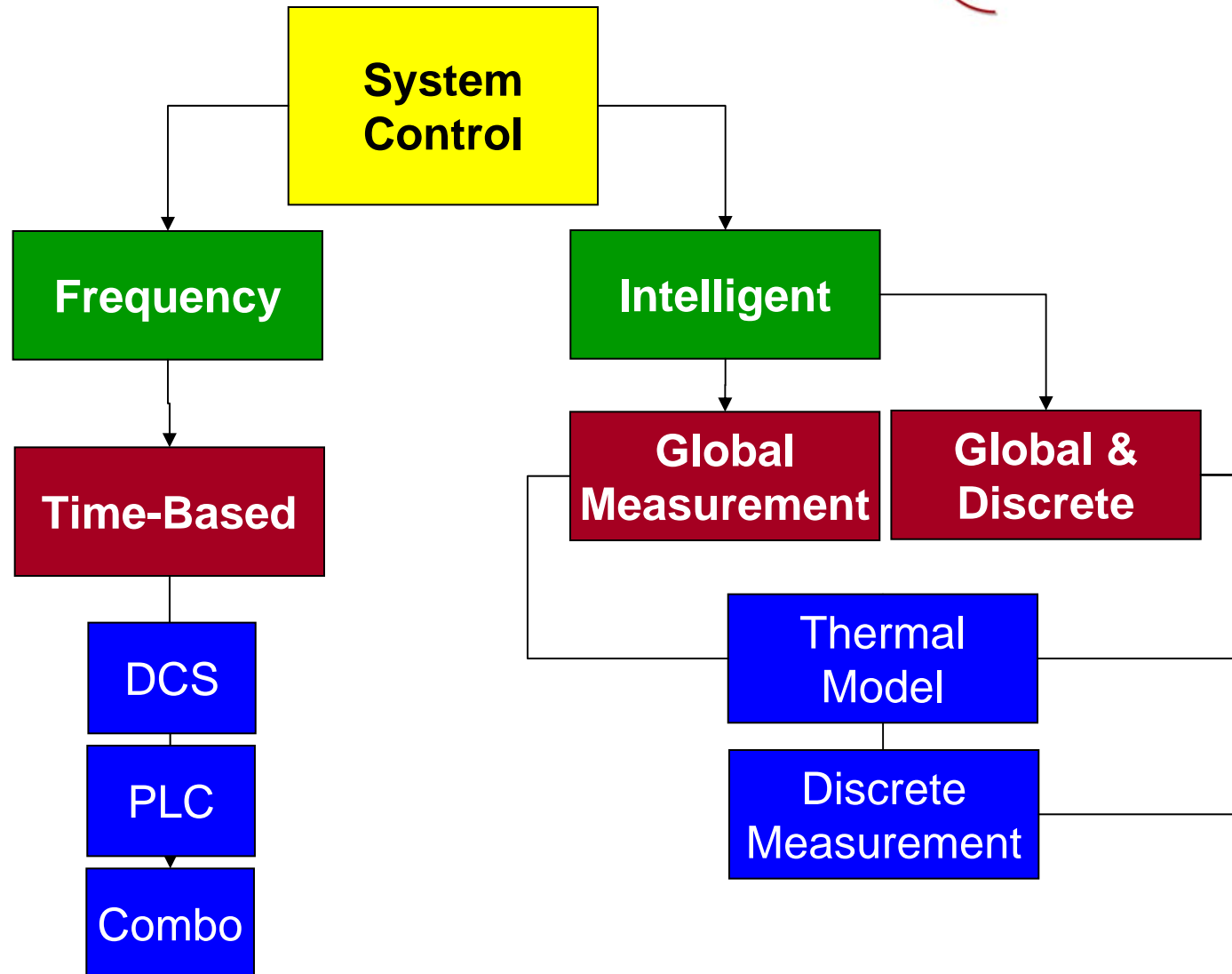
SmartCannon
Safe, precise cleaning of furnace walls from hoppers to nose arch



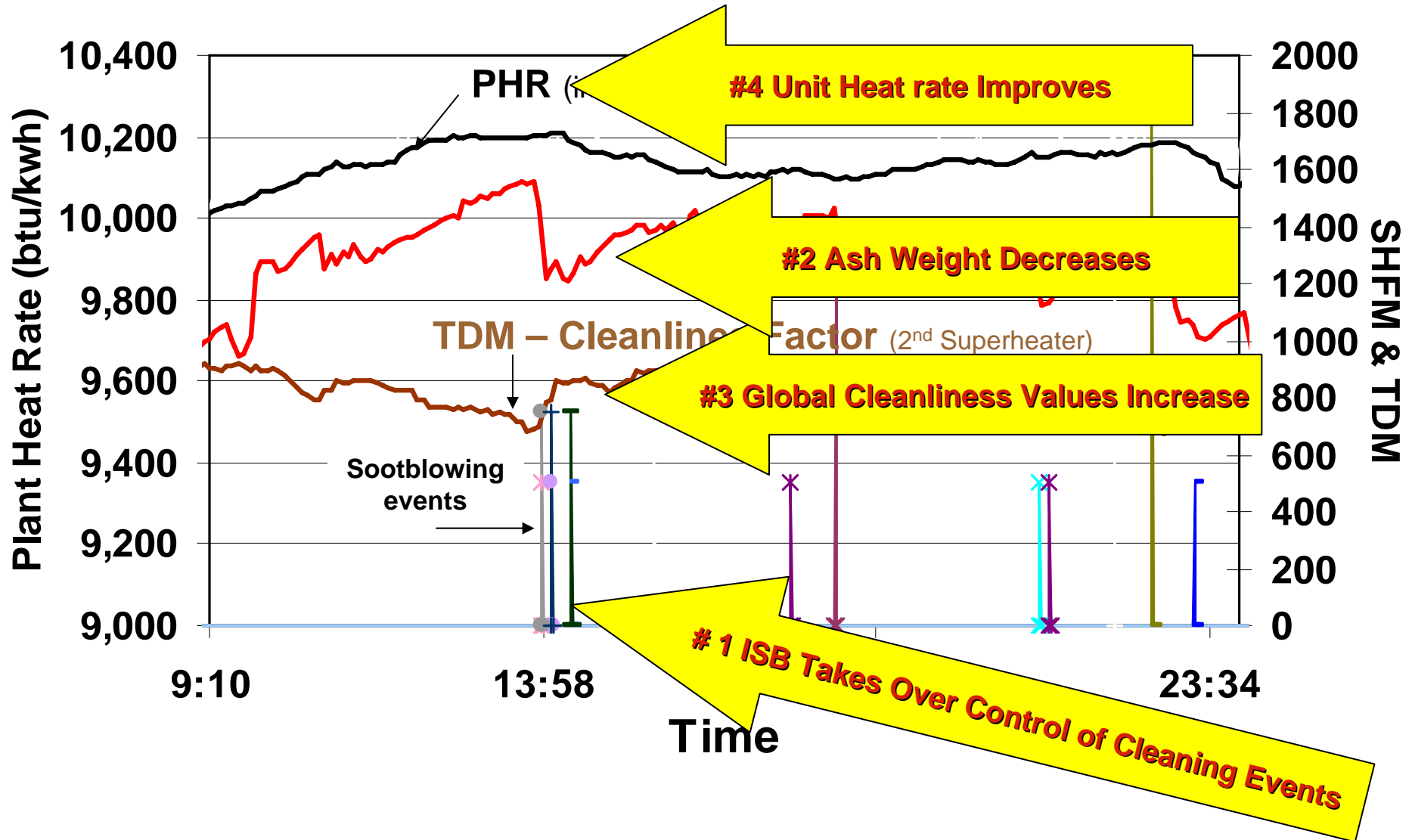
WS
Precision Water Lance



VS
Severe-Duty furnace wallblower



Relationship Cleanliness:Heat Rate



In Practice – Actual ISB Results



Post – LNB, OFA and Fuel Switch

INDIVIDUAL GENERATING BANK CLEANLINESS VALUES

Cleanliness Coefficient	Platen SH	SSH	RH OUT	Pri SH	RH IN	ECO
24 hours after stop ISB	91	91	85	95	90	97
24 Hours after resume ISB	93	93	87	97	93	99
Net Change	2%	2%	2%	2%	3%	2%

Cleanliness Factors Improved For ALL Zones

AVERAGE HEAT FLUX (2 HRS)

24 Hours after stop ISB	50	k/Btu/sqft/hr
24 hours after resume ISB	54	k/Btu/sqft/hr
Net Change	8%	

Furnace Heat Flux Improved

AVERAGE FEGT (2 HRS)

24 Hours after stop ISB	2545	F
24 hours after resume ISB	2505	F
Net Change	-2%	

40° F Reduction In FEGT

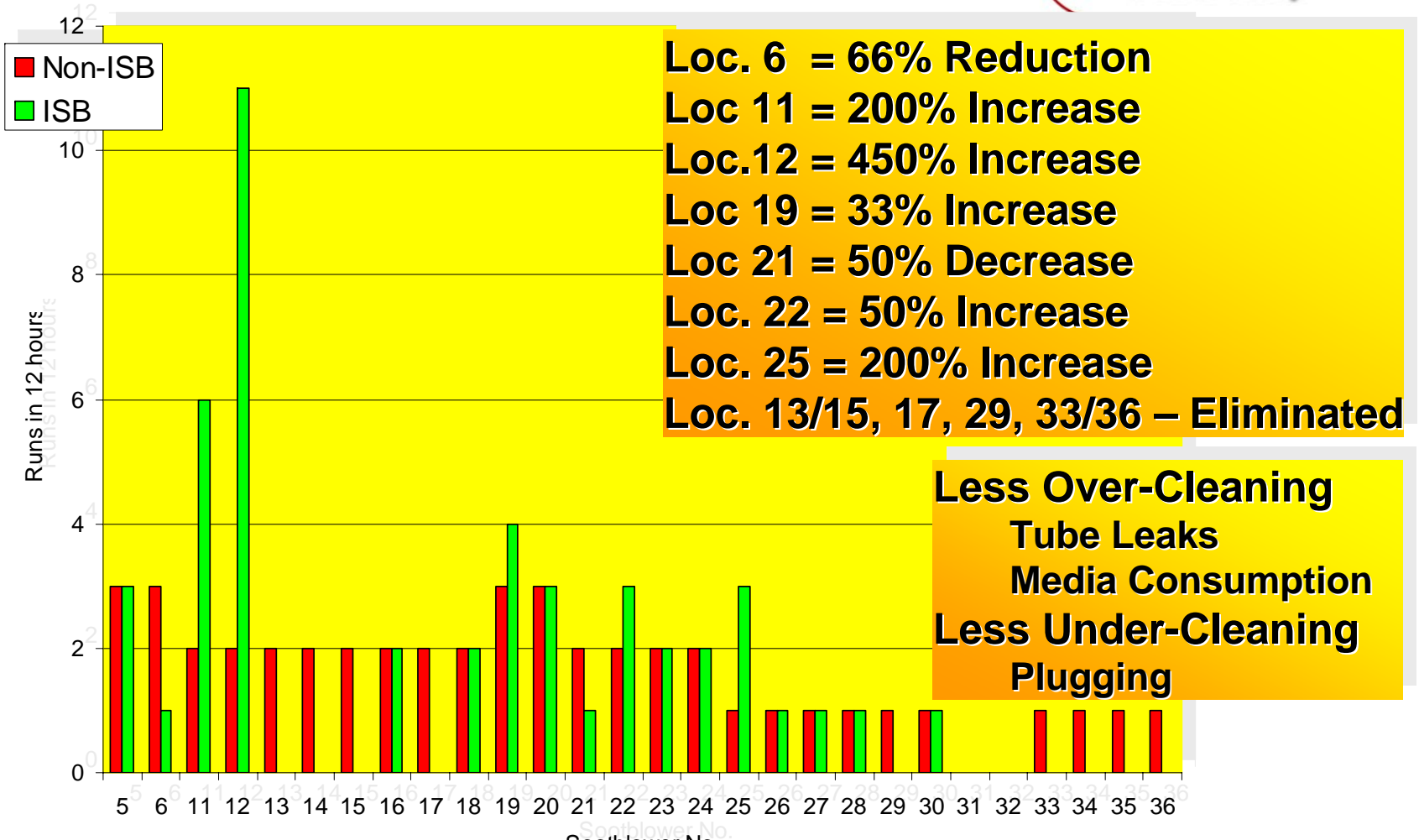
AVERAGE RH SPRAY FLOW (12 hours)

ISB not in service	27	k/pph
ISB in service	21	k/pph
Net Change	-23%	

Substantial Spray Flow Reduction

24 HOUR BASELINE TEST NORMAL SEQUENTIAL OPERATION VS. ISB OPERATION

In Practice – Actual ISB Results



To Achieve These Results the ISB System Dramatically Altered Individual Sootblower Frequencies Based on Real-Time Conditions

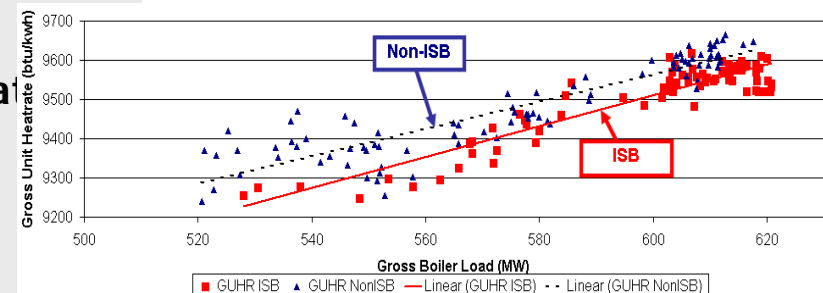
Case Study: Heat Rate Improvement



- NRG Big Cajun Unit 3
- 630 MW B&W Boiler
- Fuel: PRB Coal
- Challenges: Severe slagging causing unplanned outages
- Solution: SmartClean System installed
 - Automated Cleaning
 - Fouling Sensors in Furnace and Super heater
 - SmartCannon for furnace cleaning



- Annual Benefits:
 - 1% Heat rate improvement \$1M
 - Eliminate outage \$3M^{yr}
 - Total \$4M
- Payback: Less Than 1 year



PHR Improvement = 9590 – 9500 = 90 Btu/KWh

Power saved = 90 Btu/KWh * 1000 KWh/MWh * 600 MW = 57.10⁶

Cost reduction = 57.10⁶ Btu/hr * 1KWh/9500Btu * 1000kwh/MWh * **\$20/MWh**

= **\$968,589 per year (355 days)**

Justification Tools Available



- Quantify individual plant situation
- Establish discounted cash flow analysis

Net Present Value (NPV) Calculator for Boiler Cleaning Projects

Project:		John Doe Power Station - Water Cannons										
Cost of Capital		10%										
Year:		1	2	3	4	5	6	Total				
Capital Equipment	\$	(650,000)	\$	-	\$	-	\$	-	\$	(650,000)		
Labor	\$	(350,000)							\$	(350,000)		
Other Capital Costs												
Incremental Operating Costs	\$	-	\$	-	\$	-	\$	-	\$	-		
Total Outflows	\$	(1,000,000)	\$	-	\$	-	\$	-	\$	(1,000,000)		
Operating Profit from Incremental												
Generation	\$	875,000	\$	875,000	\$	875,000	\$	875,000	\$	875,000	\$	5,250,000
Avoided Outage Costs	\$	220,000	\$	220,000	\$	220,000	\$	220,000	\$	220,000	\$	1,320,000
Fuel Savings From Improved Heat Rate	\$	500,000	\$	500,000	\$	500,000	\$	500,000	\$	500,000	\$	3,000,000
Fuel Savings From Lower Fuel Price	\$	2,500,000	\$	2,500,000	\$	2,500,000	\$	2,500,000	\$	2,500,000	\$	15,000,000
Avoided Ammonia Cost	\$	65,000	\$	65,000	\$	65,000	\$	65,000	\$	65,000	\$	390,000
Avoided Catalyst Replacement	\$	140,000	\$	140,000	\$	140,000	\$	140,000	\$	140,000	\$	840,000
Avoided NOx Credit Cost	\$	-	\$	-	\$	-	\$	-	\$	-	\$	-
Avoided Media Costs	\$	35,000	\$	35,000	\$	35,000	\$	35,000	\$	35,000	\$	210,000
Other	\$	-	\$	-	\$	-	\$	-	\$	-	\$	-
Depreciation Rate		40%		30%		20%		5%		3%		3%
Depreciation	\$	400,000	\$	300,000	\$	200,000	\$	50,000	\$	25,000	\$	1,000,000
Corporate Tax Rate		30%		30%		30%		30%		30%		30%
Corporate Tax	\$	(1,180,500)	\$	(1,210,500)	\$	(1,240,500)	\$	(1,285,500)	\$	(1,293,000)	\$	(7,503,000)
Total Inflows	\$	3,154,500	\$	3,124,500	\$	3,094,500	\$	3,049,500	\$	3,042,000	\$	18,507,000
Cash Flow	\$	2,154,500	\$	3,124,500	\$	3,094,500	\$	3,049,500	\$	3,042,000	\$	17,507,000
6-yr Discounted Cash Flow - NPV/IRR	\$	1,958,636	\$	2,582,231	\$	2,324,944	\$	2,082,850	\$	1,888,843	\$	12,554,633
6-yr Return on Investment - ROI	1255%											
Payback Period	0.48	Years										

Boiler Cleanliness Configurator						Commercial Release Revision 1.3	
1.0	Plant:	Mirant Chalk Point			Unit #:	1 and 2	
2.0	Driver	Value	U/M	Day	Month	Year	
3.0	Plant Data						
4.0	Production Data						
5.0	Capacity:	355	Mw	Boiler Mfg:	BW		
6.0	Demand Factor:	85%		Boiler Type:	Supercritical		
7.0	Average Demand:	302	Mwh	7,242	220,273	2,643,272	
8.0	Steam Production:	2,196,740	PPH	52,721,760	1,603,585,052	19,243,020,626	
9.0	Feedwater Flow:	3,207,240	PPH	Type of Air Preheater:		Dual Regenerative	
10.0	Wheeled Revenue Potential:	\$ 70.00	Mwh	\$ 506,940	\$ 15,419,087	\$ 185,029,044	
10.1	Avg Replacement Power Cost:	\$ 40.00	Mwh				
11.0	Sootblower Compliment						
12.0	Cleaning Media:	Steam	360	PSIG	575	F	
13.0		Qty	Travel(*)	Model	Cycles per Day	Media Consumption per Day	
14.0	Wallblower:	42	1.0	IR	3	10,710	
15.0	Average Availability:	95%					
16.0	Water Lance:	0					
17.0	Average Availability:						
18.0	Water Cannon:	0					
19.0	Average Availability:						
20.0	Full Retract:	20	25.0	IK525	2	64,615	
21.0	Average Availability:	90%					
22.0	1/2 Retract:						
23.0	Average Availability:	90%					
24.0	APH:	2	10.0	Retractable	6	25,200	
25.0	Sonic:	0					
26.0	Daily Cleaning Media Consumption (lbs for steam blowing and scf for air blowing)						100,525

Thank You

